

## METHOD FOR MANUFACTURING A POLYHYDROXYALKANOATE

This application is a division of Application No.  
5 09/951,720, filed on September 14, 2001, which is  
incorporated herein by reference.

### BACKGROUND OF THE INVENTION

#### Field of the Invention

10 The present invention relates to a novel  
polyhydroxyalkanoate (hereinafter, sometimes abbreviated as  
PHA) and also to a method for manufacturing PHA very  
efficiently using a microorganism having capability to  
produce the PHA and accumulate it in bacterial bodies.

15 In addition, the present invention relates to a method  
for producing PHA using a substituted alkane derivative as a  
raw material.

#### Related Background Art

It has been reported so far that a variety of  
20 microorganisms produce poly-3-hydroxybutyric acid  
(hereinafter, sometimes abbreviated as PHB) and other PHAs  
and accumulate them in bacterial bodies ("Handbook of  
Biodegradable Plastic", edited by Research Association of  
Biodegradable Plastic, NTS Co., Ltd., pp.178-197). These  
25 polymers as well as conventional plastics can be utilized  
for production of various products by melt processing or the  
like. Further, the polymers are biodegradable, and  
therefore they have an advantage of being completely  
degraded by microorganisms in nature, and causing no  
30 pollution by being left in natural environment unlike many

conventional synthetic polymer compounds. Further, they are also excellent in biocompatibility and expected to be applied to a medical soft member or the like.

5           It has been known that such PHA produced by a microorganism may have a variety of compositions and structures depending on types of microorganism, culture medium composition, culture conditions and the like, and mainly from the viewpoint of improving physical  
10       properties of PHA, the study has been performed so far for controlling such composition and structure.

          <<1>> First, the biosynthesis of PHAs which are obtained by polymerizing monomer units with a relatively simple structure such as 3-hydroxybutyric  
15       acid (hereinafter, sometimes abbreviated as 3HB) includes the followings.

          For example, it is reported that *Alcaligenes eutropus* H16 strain (ATCC No. 17699) and its variants produce copolymers of 3-hydroxybutyric acid and 3-  
20       hydroxyvaleric acid in various composition ratios with a carbon source varied in their culturing (U.S. Patent Nos. 4,393,167 and 4,876,331).

          In U.S. Patent No. 5,200,332, a method for producing copolymers of 3-hydroxybutyric acid and 3-  
25       hydroxyvaleric acid by making a microorganism of *Methylobacterium* sp., *Paracoccus* sp., *Alcaligenes* sp., or *Pseudomonas* sp. contact a primary alcohol having 3

to 7 carbons is disclosed.

In U.S. Patent No. 5,292,860 and Japanese Patent Application Laid-Open No. 7-265065, it is disclosed that a two-component copolymer of 3-hydroxybutyric acid and 3-hydroxyhexanoic acid is produced by culturing  
5 Aeromonas caviae using oleic acid and olive oil as carbon sources.

In Japanese Patent Application Laid-Open No. 9-191893, it is disclosed that a polyester having monomer  
10 units of 3-hydroxybutyric acid and 4-hydroxybutyric acid is produced by culturing Comamonas acidovorans IFO 13852 strain using gluconic acid and 1,4-butanediol as carbon sources.

Recently, studies on a PHA comprising a 3-  
15 hydroxyalkanoic acid having medium-chain-length (abbreviated as mcl) wherein the number of carbons is up to about 12 have been carried out energetically. The synthetic route of such PHAs can be roughly classified into two parts, specifically examples of  
20 which will be shown in the following (1) and (2).

(1) Synthesis using  $\beta$ -oxidation:

In U.S. Patent No. 5,135,859, it is disclosed that a PHA having a monomer unit of 3-hydroxyalkanoic acid having 6 to 12 carbons is produced by supplying an  
25 acyclic aliphatic hydrocarbon as a carbon source to Pseudomonas oleovorans ATCC 29347 strain. In Appl. Environ. Microbiol., 58 (2), 746 (1992), it is reported

that *Pseudomonas resinovorans* produces a polyester with monomer units of 3-hydroxybutyric acid, 3-hydroxyhexanoic acid, 3-hydroxyoctanoic acid and 3-hydroxydecanoic acid (the amount ratio: 1 : 15 : 75 : 9) using octanoic acid as a sole carbon source, and further a polyester with monomer units of 3-hydroxybutyric acid, 3-hydroxyhexanoic acid, 3-hydroxyoctanoic acid and 3-hydroxydecanoic acid (the amount ratio: 8 : 62 : 23 : 7) using hexanoic acid as a sole carbon source. Herein, it is considered that a monomer unit of a 3-hydroxyalkanoic acid having longer chain than that of a fatty acid as a material passes through the synthetic route of the fatty acid described in (2).

(2) Synthesis using fatty acid de novo biosynthesis

In Int. J. Biol. Macromol., 16 (3), 119 (1994), it is reported that *Pseudomonas* sp. 61-3 strain produces a polyester with monomer units of 3-hydroxyalkanoic acids such as 3-hydroxybutyric acid, 3-hydroxyhexanoic acid, 3-hydroxyoctanoic acid, 3-hydroxydecanoic acid and 3-hydroxydodecanoic acid, and of 3-hydroxyalkenic acids such as 3-hydroxy-5-cis-decenic acid and 3-hydroxy-5-cis-dodecenic acid using sodium gluconate as a sole carbon source.

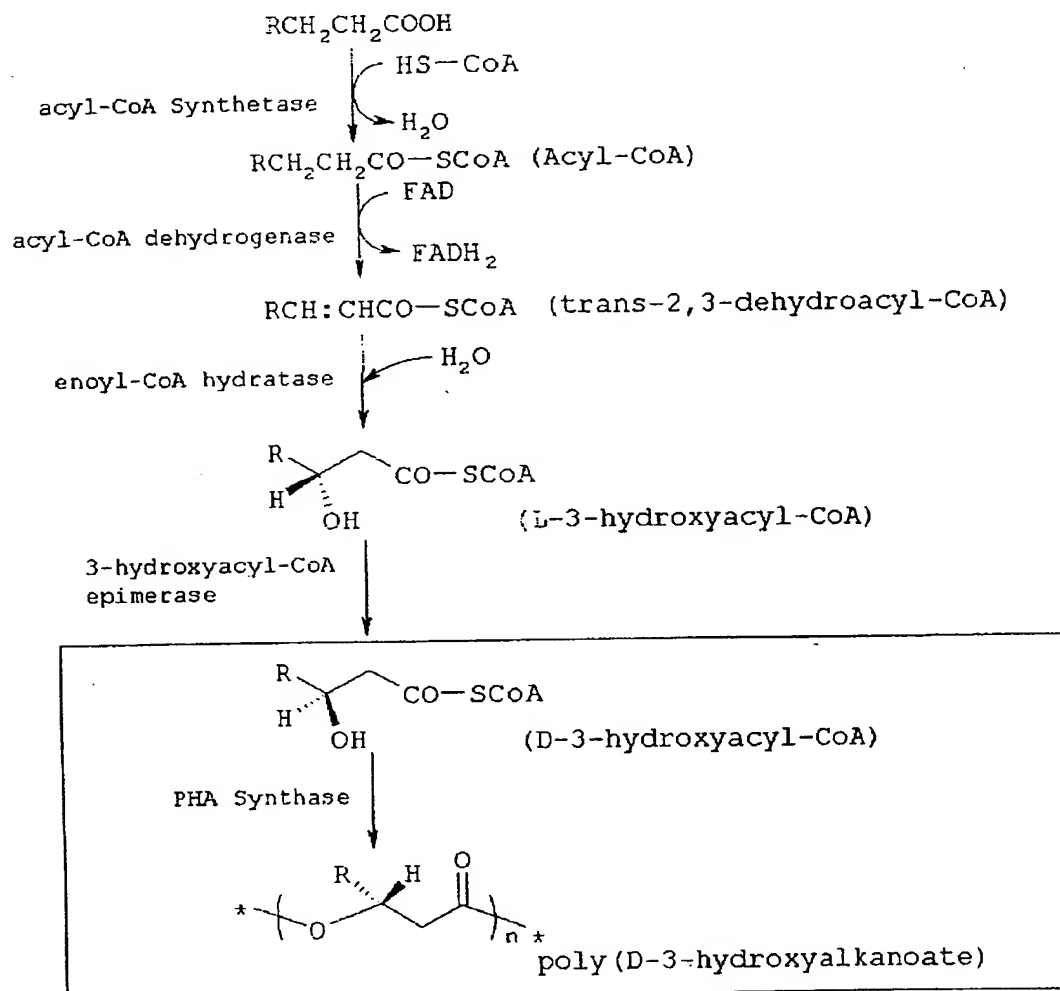
By the way, the biosynthesis of PHA is usually performed by PHA synthase using "D-3-hydroxyacyl-CoA" as a substrate which is generated as an intermediate of



various metabolic pathways in the cells.

Herein, "CoA" means "coenzyme A". As described in the prior art of the above (1), when using a fatty acid such as octanoic acid, nonanoic acid or the like as a carbon source, it is said that the biosynthesis of PHA is carried out using "D-3-hydroxyacyl-CoA" as a starting material which is generated during the "β-oxidation pathway".

The reactions until PHA is biosynthesized through "β-oxidation pathway" are shown below.



On the other hand, as described in the prior art of the above described (2), when PHA is biosynthesized using saccharides such as glucose or the like, it is said that the biosynthesis is carried out using "D-3-hydroxyacyl-CoA" as a starting material converted from "D-3-hydroxyacyl-ACP" which is generated in the "fatty acid de novo biosynthesis"

Herein, "ACP" means "acyl carrier protein".

By the way, any of PHAs synthesized in the above (1) and (2) as described above is PHA which comprises monomer units having an alkyl group in the side chain, i.e. "usual PHA".

<<2>> However, when considering application of such PHAs produced by a microorganism to a wider range, e.g. as a functional polymer, PHAs ("unusual PHAs") in which

substituents other than an alkyl group are introduced into the side chain are expected to be extremely useful.

Examples of the substituent include those containing an aromatic ring (such as a phenyl group, a phenoxy group, a benzoyl group or the like), an unsaturated hydrocarbon, an ester group, an aryl group, a cyano group, a halogenated hydrocarbon, an epoxide or the like. Of them, PHAs having an aromatic ring have been studied extensively.

(a) Those containing a phenyl group or its partially substituted form

In Makromol. Chem., 191, 1957-1965 (1990) and Macromolecules, 24, 5256-5260 (1991), it is reported that *Pseudomonas oleovorans* produces PHA containing 3-hydroxy-5-phenylvaleric acid as a unit using 5-phenylvaleric acid as a substrate.

Specifically, it is reported that *Pseudomonas oleovorans* produces 160 mg (31.6% of the dry weight to the bacterial body) per liter of a culture solution of a PHA comprising 3-hydroxyvaleric acid, 3-hydroxyheptanoic acid, 3-hydroxynonanoic acid, 3-hydroxyundecanoic acid and 3-hydroxy-5-phenylvaleric acid in a ratio of 0.6 : 16.0 : 41.1 : 1.7 : 40.6 as monomer units using 5-phenylvaleric acid and nonanoic acid as substrates (molar ratio of 2 : 1, total concentration of 10 mmol/L), and also this produces 200 mg (39.2% of the dry weight to the bacterial body) per liter of a culture solution of PHA containing 3-hydroxyhexanoic acid, 3-hydroxyoctanoic acid, 3-hydroxydecanoic acid and 3-hydroxy-5-phenylvaleric acid in a ratio of 7.3 : 64.5 : 3.9 : 24.3 as monomer units using 5-phenylvaleric acid and octanoic acid as substrates (molar ratio of 1 : 1, total concentration of 10 mmol/L). It is considered that the PHAs in this report is synthesized mainly through the  $\beta$ -oxidation pathway because nonanoic acid and octanoic acid are used.

The relating description is in Chirality, 3, 492-494 (1991) besides the above where change in the physical properties of the polymer is recognized which

is presumably caused by containing a 3-hydroxy-5-phenylvaleric acid unit.

In *Macromolecules*, 29, 1762-1766 (1996), it is reported that *Pseudomonas oleovorans* produces a PHA  
5 containing 3-hydroxy-5-(4'-tolyl)valeric acid as a unit using 5-(4'-tolyl)valeric acid as a substrate.

In *Macromolecules*, 32, 2889-2895 (1999), it is reported that *Pseudomonas oleovorans* produces a PHA  
10 containing 3-hydroxy-5-(2',4'-dinitrophenyl)valeric acid and 3-hydroxy-5-(4'-nitrophenyl)valeric acid as units using 5-(2',4'-dinitrophenyl)valeric acid as a substrate.

(b) Those containing a phenoxy group or the partially substituted form

15 In *Macromol. Chem. Phys.*, 195, 1665-1672 (1994), it is reported that *Pseudomonas oleovorans* produces a PHA copolymer of 3-hydroxy-5-phenoxyvaleric acid and 3-hydroxy-9-phenoxyundecanoic acid using  
11-phenoxyundecanoic acid as a substrate.

20 Also in *Macromolecules*, 29, 3432-3435 (1996), it is reported that using *Pseudomonas oleovorans*, a PHA comprising 3-hydroxy-4-phenoxybutyric acid and 3-hydroxy-6-phenoxyhexanoic acid as units is produced  
from 6-phenoxyhexanoic acid, a PHA comprising  
25 3-hydroxy-4-phenoxybutyric acid, 3-hydroxy-6-phenoxyhexanoic acid and 3-hydroxy-8-phenoxyoctanoic acid as units is produced from 8-phenoxyoctanoic acid,

and a PHA comprising 3-hydroxy-5-phenoxyvaleric acid and 3-hydroxy-7-phenoxyheptanoic acid as units is produced from 11-phenoxyundecanoic acid. Some of polymer yields in this report are excerpted as follows.

5 [Table 1]

	Carbon source (alkanoate)	Dry cell weight (mg/L)	Dry polymer weight (mg/L)	Yield (%)
	6-Phenoxyhexanoic acid	950	100	10.5
	8-Phenoxyoctanoic acid	820	90	11
10	11-Phenoxyundecanoic acid	150	15	10

In Japanese Patent Publication No. 2989175, a homopolymer comprising a 3-hydroxy-5-  
15 (monofluorophenoxy)pentanoate (3H5(MFP)P) unit or a 3-hydroxy-5-(difluorophenoxy)pentanoate (3H5(DFP)P) unit, a copolymer comprising at least 3H5(MFP)P unit or 3H5(DFP)P unit, *Pseudomonas putida* capable of synthesizing these polymers, and the invention relating  
20 to a method for manufacturing the above described polymers where *Pseudomonas* genus is used is disclosed.

These production is performed by the following "two-step culture".  
Culture time: 24 hours for the 1st step; and 96 hours  
25 for the 2nd step.

The substrates and polymers obtained in each step are shown as follows.

(1) Polymer obtained: 3-hydroxy-5-(monofluorophenoxy)pentanoate homopolymer

Substrate in the 1st step: citric acid, yeast extract

5 Substrate in the 2nd step:  
monofluorophenoxyundecanoic acid

(2) Polymer obtained: 3-hydroxy-5-(difluorophenoxy)pentanoate homopolymer

10 Substrate in the 1st step: citric acid, yeast  
extract

Substrate in the 2nd step:  
difluorophenoxyundecanoic acid

(3) Polymer obtained: 3-hydroxy-5-(monofluorophenoxy)pentanoate copolymer

15 Substrate in the 1st step: octanoic acid or  
nonanoic acid, yeast extract

Substrate in the 2nd step:  
monofluorophenoxyundecanoic acid

20 (4) Polymer obtained: 3-hydroxy-5-(difluorophenoxy)pentanoate copolymer

Substrate in the 1st step: octanoic acid or  
nonanoic acid, yeast extract

Substrate in the 2nd step:  
difluorophenoxyundecanoic acid.

25 It is said that as the effect, the polymer having  
a phenoxy group substituted with one or two fluorine  
atoms at the end of side chain can be synthesized by  
assimilating a medium chain fatty acid having a

substituent, and the stereoregularity and water repellency can be provided while keeping good workability with a high melting point.

Compounds substituted with cyano and nitro groups  
5 other than such forms substituted with such a fluoro group have also been studied.

In Can. J. Microbiol., 41, 32-43 (1995) and Polymer International, 39, 205-213 (1996), it is reported that using *Pseudomonas oleovorans* ATCC 29347  
10 strain and *Pseudomonas putida* KT 2442 strain, PHA comprising 3-hydroxy-p-cyanophenoxyhexanoic acid or 3-hydroxy-p-nitrophenoxyhexanoic acid as a monomer unit is produced using octanoic acid and p-cyanophenoxyhexanoic acid or p-nitrophenoxyhexanoic  
15 acid as substrates.

In these reports, since any polymer has an aromatic ring at the side chain of PHA which is different from general PHA having an alkyl group at the side chain, it will be advantageous to obtain polymers  
20 having the physical properties originated in them.

(c) PHA containing a cyclohexyl group in the monomer unit is expected to exhibit the physical properties of the macromolecule which is different from that of PHAs comprising usual aliphatic hydroxyalkanoic acid as units, and an example of the production by  
25 *Pseudomonas oleovorans* is reported (Macromolecules, 30, 1611-1615 (1997)).

According to this report, *Pseudomonas oleovorans* is cultivated in the culture medium wherein nonanoic acid and cyclohexylbutyric acid or cyclohexylvaleric acid coexist, and the resulting PHA comprises a unit containing a cyclohexyl group and a unit originated from nonanoic acid (each ratio is unknown).

For the yield etc., it is reported that the results shown in Table 2 were obtained by varying the ratio of cyclohexylbutyric acid and nonanoic acid in the condition of 20 mmol/L of the substrate concentration in total to cyclohexylbutyric acid.

[Table 2]

Nonanoic acid:cyclohexylbutyric acid	CDW	PDW	Yield	Unit
5:5	756.0	89.1	11.8	Nonanoic acid, cyclohexylbutyric acid
1:9	132.8	19.3	14.5	Nonanoic acid, cyclohexylbutyric acid

CDW: dry cell weight (mg/L), PDW: dry polymer weight (mg/L), Yield: PDW/CDW (%).

However, this example shows that the yield of the polymer per culture solution is insufficient, and also that the PHA itself obtained is mixed with the aliphatic hydroxyalkanoic acid originated in nonanoic acid in the monomer unit.

<<3>> Further, as a new category, the study is performed not only on the change of the physical properties but also for producing PHA having an



appropriate functional group on the side chain to create a new function utilizing the functional group.

For example, in *Macromolecules*, 31, 1480-1486 (1996) and *Journal of Polymer Science: Part A: Polymer Chemistry*, 36, 2381-2387 (1998), etc., it is reported  
5 that PHA comprising a unit having a vinyl group at the end of the side chain was synthesized, then epoxidated with an oxidizing agent resulting in the synthesis of PHA containing a highly reactive epoxy group at the end  
10 of the side chain.

Further, as a synthetic example of PHA comprising a unit which has a sulfide expected to be highly reactive others than the vinyl group, it is reported in  
15 *Macromolecules*, 32, 8315-8318 (1999) that *Pseudomonas putida* 27N01 strain produces a PHA copolymer of 3-hydroxy-5-(phenylsulfanyl)valeric acid and 3-hydroxy-7-(phenylsulfanyl)heptanoic acid using 11-phenylsulfanylvaleric acid as a substrate.

As described above, while different compositions  
20 and structures of PHAs produced by microorganisms are obtained by varying types of microorganisms and composition of the culture medium, conditions of the culture and the like used for their production, it is not said yet to be sufficient for the physical  
25 properties when considering application as plastic. In order to further increase the use extent of the PHA produced by microorganisms, it is important to examine

improvement of the physical properties more widely, and therefore it is essential to develop and explore PHAs comprising monomer units having further various structures and their manufacturing methods and  
5 microorganisms which can produce the desired PHA efficiently.

Moreover, in a typical producing method of PHA consisting of giving a microorganism a chemically synthesized substituted fatty acid as a substrate,  
10 there are many cases where a significant limitation on a chemical synthesis is imposed depending on the type, number, position and the like of a substituent to be introduced, since the carboxyl group of the substituted fatty acid is an active group in a chemical reaction,  
15 or because of the active group, complex handling such as protection and deprotection of the carboxyl group in the reaction steps of the chemical synthesis is required, and chemical reactions over several steps in the process are often required. Therefore, there was  
20 difficulty of the synthesis on an industrially producing level or requirement for much time, troubles and costs for the synthesis.

On the other hand, if "unusual PHA" can be produced using a substituted alkane, which is more  
25 easily synthesized chemically than substituted fatty acid, as a material, it is assumed that the above problems could be solved.

For production of PHA from alkane derivatives which have been reported so far, there are only examples that the corresponding PHAs were biosynthesized by microorganisms using straight chain alkanes and alkenes (alkanes containing double bonds) (Appl. Environ. Microbiol., 54, 2924-2932 (1988)), chlorine-substituted alkanes (Macromolecules, 23, 3705-3707 (1990)), fluorine-substituted alkanes (Biotechnol. Lett., 16, 501-506 (1994)) and alkanes containing acetoxymy residues (Macromolecules, 33, 8571-8575 (2000)) as starting materials, whereas there are no synthetic examples of the corresponding PHAs from an alkane having a residue containing an aromatic ring as a substituent reported.

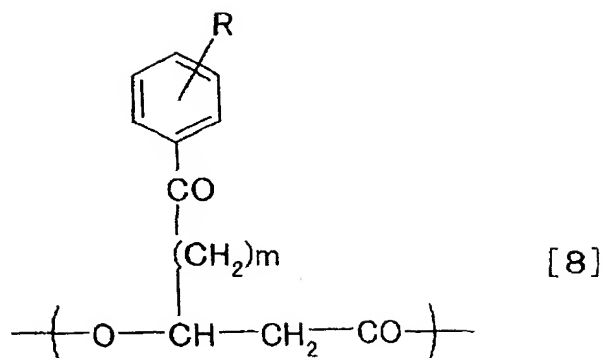
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#### SUMMARY OF THE INVENTION

Therefore, the present inventors have studied assiduously on exploration of microorganisms having capability of producing different PHAs and accumulating them in the bacterial body and on a producing method of desired PHAs using such microorganisms, aiming at development of PHAs having a functional group at the side chain useful for a device material, a medical material and the like. Consequently, there was found a microorganism capable of producing a novel PHA comprising a 3-hydroxy-substituted benzoylalkanoic acid unit represented by the chemical

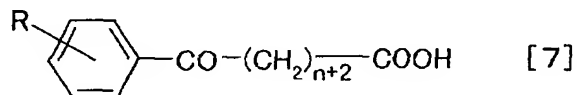
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formula [8]:



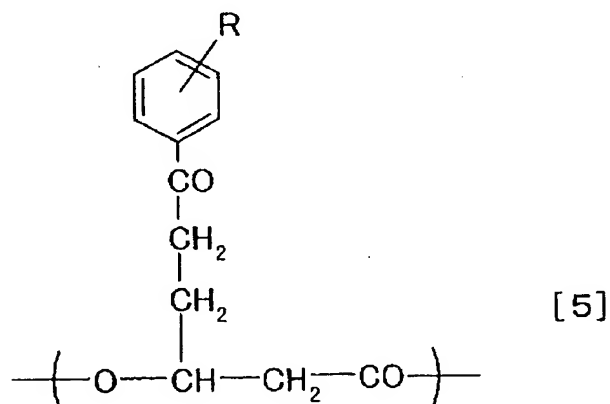
wherein m is at least one or more selected from the group consisting of n, n-2, n-4 and n-6 and one or more of integers; n is any integer of 1 to 8 corresponding to n in the following chemical formula [7]; and R is any one selected from the group consisting of a halogen atom, -CN, -NO<sub>2</sub>, -CH<sub>3</sub>, -C<sub>2</sub>H<sub>5</sub>, -C<sub>3</sub>H<sub>7</sub>, -CF<sub>3</sub>, -C<sub>2</sub>F<sub>5</sub> and -C<sub>3</sub>F<sub>7</sub>, corresponding to R in chemical formula [7], using a substituted benzoylalkanoic acid represented by chemical formula [7] as a material:

[7]

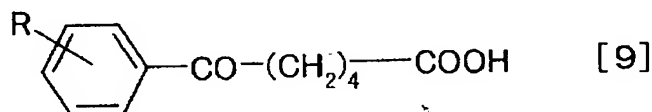


wherein n is any integer of 1 to 8; and R is any one selected from the group consisting of a halogen atom, -CN, -NO<sub>2</sub>, -CH<sub>3</sub>, -C<sub>2</sub>H<sub>5</sub>, -C<sub>3</sub>H<sub>7</sub>, -CF<sub>3</sub>, -C<sub>2</sub>F<sub>5</sub> and -C<sub>3</sub>F<sub>7</sub>, and of accumulating it in the bacterial body. It was further found that the PHA can be biosynthesized by

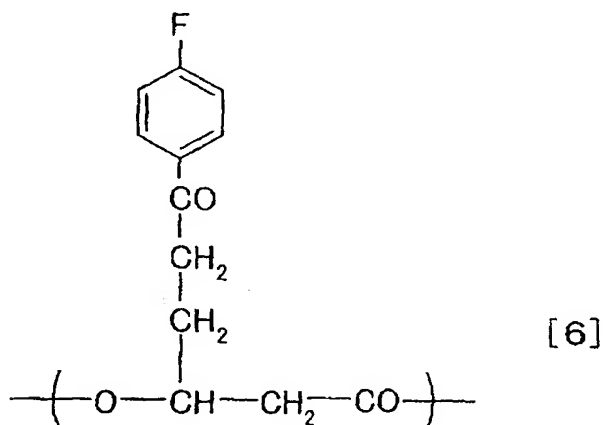
culturing the microorganism under coexistence of the substituted benzoylalkanoic acid represented by the above chemical formula [7] with saccharides, an organic acid involved in the TCA cycle, yeast extract or polypeptone, and that the resulting PHA has relatively high purity. Specifically, for example, there was found a microorganism capable of producing a novel PHA comprising a 3-hydroxy-substituted benzoylvaleric acid unit represented by the chemical formula [5]:



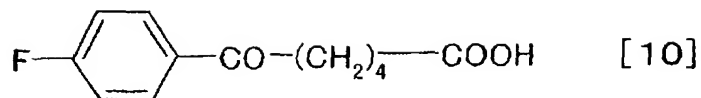
wherein R is any one selected from the group consisting of a halogen atom, -CN, -NO<sub>2</sub>, -CH<sub>3</sub>, -C<sub>2</sub>H<sub>5</sub>, -C<sub>3</sub>H<sub>7</sub>, -CF<sub>3</sub>, -C<sub>2</sub>F<sub>5</sub> and -C<sub>3</sub>F<sub>7</sub>, corresponding to R in the following chemical formula [9], using a substituted benzoylvaleric acid represented by chemical formula [9] as a material:



wherein R is any one selected from the group consisting of a halogen atom, -CN, -NO<sub>2</sub>, -CH<sub>3</sub>, -C<sub>2</sub>H<sub>5</sub>, -C<sub>3</sub>H<sub>7</sub>, -CF<sub>3</sub>, -C<sub>2</sub>F<sub>5</sub> and -C<sub>3</sub>F<sub>7</sub>, and capable of accumulating it in the bacterial body. It was further found that the PHA can be biosynthesized by culturing the microorganisms under coexistence of the substituted benzoylvaleric acid represented by the above chemical formula [9] with saccharides, an organic acid involved in the TCA cycle, yeast extract or polypeptone, and that the resulting PHA has relatively high purity. More specifically, for example, there was found a microorganism capable of producing a novel PHA comprising a 3-hydroxy-5-(4-fluorobenzoyl)valeric acid unit (hereinafter, sometimes abbreviated as 3HFBzV) represented by chemical formula [6]:

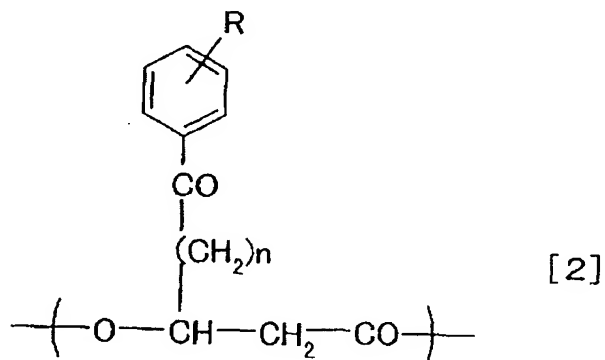


using 5-(4-fluorobenzoyl)valeric acid (hereinafter, abbreviated as FBzVA) represented by chemical formula [10] as a material:



and capable of accumulating it in the bacterial body. It was further found that the PHA can be biosynthesized by culturing the microorganisms under coexistence of the substituted benzoylalkanoic acid with saccharides, an organic acid involved in the TCA cycle, yeast extract or polypeptone, and that the resulting PHA has relatively high purity, attaining the present invention.

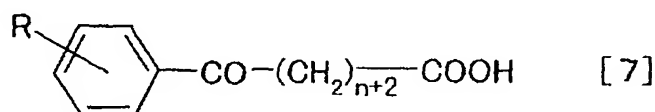
That is, the present invention relates to PHAs comprising a 3-hydroxy-substituted benzoylalkanoic acid unit as a monomer unit represented by the chemical formula [2]:



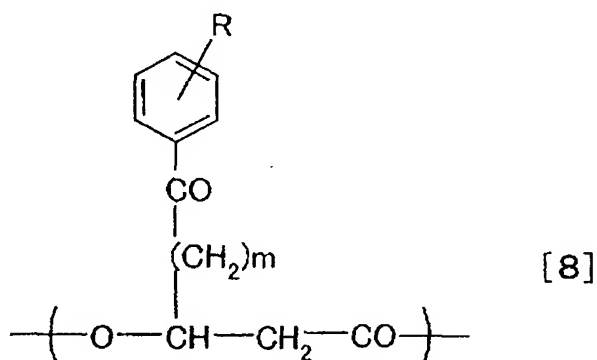
wherein n is any integer of 1 to 8; and R is any one selected from the group consisting of a halogen atom,

-CN, -NO<sub>2</sub>, -CH<sub>3</sub>, -C<sub>2</sub>H<sub>5</sub>, -C<sub>3</sub>H<sub>7</sub>, -CF<sub>3</sub>, -C<sub>2</sub>F<sub>5</sub> and -C<sub>3</sub>F<sub>7</sub>.

Further, the present invention relates to a manufacturing method of a PHA comprising the steps of culturing a microorganism in a culture medium  
5 containing a substituted benzoylalkanoic acid represented by the chemical formula [7]:



wherein n is any integer of 1 to 8; and R is any one selected from the group consisting of a halogen atom, -CN, -NO<sub>2</sub>, -CH<sub>3</sub>, -C<sub>2</sub>H<sub>5</sub>, -C<sub>3</sub>H<sub>7</sub>, -CF<sub>3</sub>, -C<sub>2</sub>F<sub>5</sub> and -C<sub>3</sub>F<sub>7</sub>, and making the microorganisms to produce the PHA comprising the corresponding 3-hydroxy-substituted benzoylalkanoic acid unit represented as the following chemical formula [8]:



wherein m is at least one or more selected from the group consisting of n, n-2, n-4 and n-6 and one or more of integers; n is any integer of 1 to 8 corresponding to n in the above chemical formula [7]; and R is any



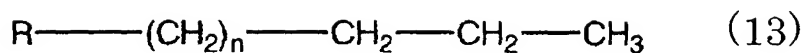
one selected from the group consisting of a halogen atom, -CN, -NO<sub>2</sub>, -CH<sub>3</sub>, -C<sub>2</sub>H<sub>5</sub>, -C<sub>3</sub>H<sub>7</sub>, -CF<sub>3</sub>, -C<sub>2</sub>F<sub>5</sub> and -C<sub>3</sub>F<sub>7</sub> corresponding to R in chemical formula [7].

That is, a method for manufacturing PHA of the present invention comprises the step of culturing a microorganism which produces PHA comprising a 3-hydroxy-substituted benzoylalkanoic acid unit under coexistence of the substituted benzoylalkanoic acid with saccharides, an organic acid involved in the TCA cycle, yeast extract or polypeptone.

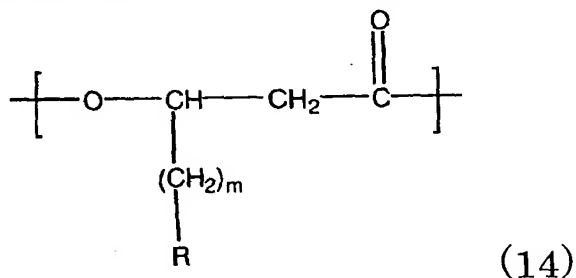
Therefore, as a result of the fact that the present inventors have examined assiduously so as to develop a producing method of "unusual PHA" using a material easier to synthesize or more readily available than substituted fatty acids, it was found that production of the "unusual PHA" is feasible using substituted alkanes as materials easier to be chemically synthesized compared with the substituted fatty acids, attaining an invention of a method for manufacturing new PHAs using the present method.

Moreover, the present invention provides a new manufacturing method of "unusual PHA".

That is, the present invention is a manufacturing method of polyhydroxyalkanoates characterized by comprising the steps of using at least one starting compound selected from the group of substituted alkanes represented by the following general formula (13):

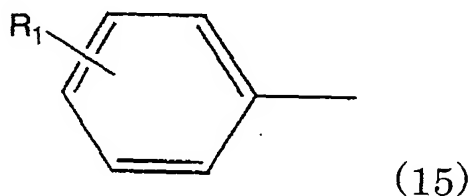


wherein R is a residue containing a substituted aromatic ring; n is an optional integer selected from 0 to 9, and of producing the polyhydroxyalkanoates comprising at least one selected from the group of 3-hydroxy-substituted alkanoate units represented by the following general formula in the molecules,



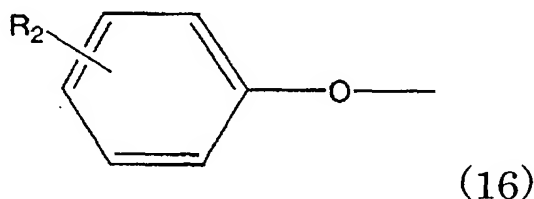
wherein R is a residue containing a substituted aromatic ring; m is any integer selected from 0 to 9.

More specifically, the manufacturing method of polyhydroxyalkanoates is characterized in that R in general formulas (13) and (14), i.e. the residue containing a substituted aromatic ring is a substituted phenyl residue group represented by the general formula (15):

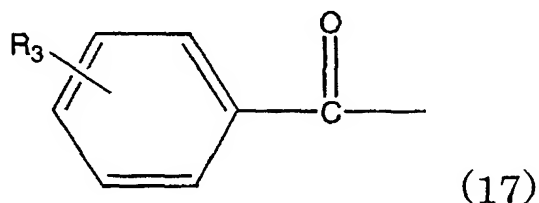


wherein R<sub>1</sub> represents a substituent on an aromatic ring.

and is at least one selected from an H atom, a CN group, an NO<sub>2</sub> group, a halogen atom, CH<sub>3</sub> group, C<sub>2</sub>H<sub>5</sub> group, C<sub>3</sub>H<sub>7</sub> group, a CH<sub>2</sub>=CH group, CF<sub>3</sub> group, C<sub>2</sub>F<sub>5</sub> group and C<sub>3</sub>F<sub>7</sub> group), a substituted phenoxy residue group represented by the general formula (16):



wherein R<sub>2</sub> represents a substituent on an aromatic ring and is at least one selected from an H atom, a CN group, an NO<sub>2</sub> group, a halogen atom, CH<sub>3</sub> group, C<sub>2</sub>H<sub>5</sub> group, C<sub>3</sub>H<sub>7</sub> group, CF<sub>3</sub> group, C<sub>2</sub>F<sub>5</sub> group and C<sub>3</sub>F<sub>7</sub> group, and a substituted benzoyl residue group represented by the general formula (17):



wherein R<sub>3</sub> represents a substituent on an aromatic ring and is at least one selected from an H atom, a CN group, an NO<sub>2</sub> group, a halogen atom, CH<sub>3</sub> group, C<sub>2</sub>H<sub>5</sub> group, C<sub>3</sub>H<sub>7</sub> group, CF<sub>3</sub> group, C<sub>2</sub>F<sub>5</sub> group and C<sub>3</sub>F<sub>7</sub> group).

The producing process of the present invention is carried out using at least one selected from a group of substituted alkanes represented by the general formula

(13) as a starting compound in the presence of the microorganism capable of producing polyhydroxyalkanoate which contains at least one selected from a group of 3-hydroxy-substituted alkanoate units represented by the general formula  
5 (14) in the molecule.

#### BRIEF DESCRIPTION OF THE DRAWINGS

Fig. 1 shows a mass spectrum of methyl 3-hydroxybutyrate when PHA obtained in the system with 1.1% amylbenzene added in  
10 Example 8 was measured by GC-MS after methanolysis treatment;

Fig. 2 shows a mass spectrum of methyl 3-hydroxyoctanoate when PHA obtained in the system with 0.1% amylbenzene added in Example 8 was measured by GC-MS after methanolysis treatment;

15 Fig. 3 shows a mass spectrum of methyl 3-hydroxydecanoate when PHA obtained in the system with 0.1% amylbenzene added in Example 8 was measured by GC-MS after methanolysis treatment:

20 Fig. 4 shows a mass spectrum of methyl 3-hydroxy-5-phenylvalerate when PHA obtained in the system with 0.1% amylbenzene added in Example 8 was measured by GC-MS after methanolysis treatment;

Fig. 5 shows a <sup>1</sup>H-NMR spectrum chart in Example 10;

Fig. 6 shows a TIC and a mass spectrum of methyl 3-

hydroxy-5-phenoxyvalerate when PHA obtained in Example 13 was measured by GC-MS after methanolysis treatment;

Fig. 7 shows a <sup>1</sup>H-NMR spectrum chart In Example 15;

Fig. 8 shows a TIC and a mass spectrum of methyl 3-hydroxy-5-(4-fluorobenzoyl)valerate when PHA obtained in Example 15 was measured by GC-MS after methanolysis treatment; and

Fig. 9 shows a <sup>1</sup>H-NMR spectrum chart in Example 16.

#### 10 DETAILED DESCRIPTION OF THE PREFERRED EMBODIMENT

PHAs of the present invention are those which comprise monomer units with various structures having substituents useful as a device material, a water repellent material, a medical material and so on at the side chain, more specifically, PHAs which have a substituted benzoyl group at the side chain. Further, the methods for manufacturing PHAs of the present invention enable manufacturing desired PHAs with high purity in a high yield by use of microorganisms. In addition, PHAs of the present invention are isotactic polymers typically composed of only R-configuration.

<Saccharides and organic acids involved in TCA cycle:  
difference from prior arts>

One of the methods for manufacturing PHAs of the

present invention is characterized in that the content rate of intended monomer units is markedly increased or only the intended monomer units exist in PHAs produced/accumulated by microorganisms by adding saccharides or organic acids

5 involved in the TCA cycle as a carbon source besides the alkanolic acid in addition to the alkanolic acid for introducing desired monomer units into the medium when culturing the microorganisms. This promoting effect of prioritizing the specific monomer unit is obtained by  
10 addition of only saccharides or organic acids involved in the TCA cycle as a carbon source besides the alkanolic acid to the medium.

In other words, the inventors obtained findings that; when saccharides or organic acids involved in the TCA cycle  
15 are cultivated as substrates coexisting with an alkanolic acid for introducing desired monomer units, intended PHAs are obtained in much higher yields with much higher purity than those obtained by conventional methods where mcl-alkanoic acids such as nonanoic acid or octanoic acid are  
20 used as a coexisting substrate; and that such effect is obtained by the fact that this culture method is capable of generating acetyl CoA which is a carbon source and an energy source of microorganisms through the method not depending on  $\beta$ -oxidation, and attained the present invention.

25 In the methods of the present invention,

saccharide compounds, e.g. glucose, fructose, mannose and the like will be used as a substrate for growth of microorganisms and a PHA produced is composed of an alkanoate for introduction of the desired monomer units coexisting with the saccharides contains no monomer units originated in the saccharides such as glucose or contain only extremely a small amount. In such a point, the methods of the present invention are basically different in both composition and effect from the conventional PHA producing methods by microorganism using saccharides themselves such as glucose as a material substrate of a monomer unit to be introduced into the PHA.

<Yeast extract: difference from conventional arts>

One of the methods for manufacturing PHAs of the present invention is characterized in that the content rate of intended monomer units is markedly increased or only the intended monomer units exist in PHAs produced/accumulated by microorganisms by adding only yeast extract as a carbon source besides the alkanoic acid in addition to the alkanoic acid for introducing desired monomer units into the medium when culturing the microorganisms. This promoting effect of prioritizing the specific monomer unit is obtained by addition of only yeast extract as a carbon source besides the alkanoic acid to the medium.

Examples of using yeast extract in the medium when

producing PHAs by microorganisms include a method using microorganisms which belong to Rhodobacter sp.

described in Japanese Patent Application Laid-Open No.

5-49487. This conventional method is, however, a

5 producing method of usual PHBs with monomer units of a hydroxyalkanoate having no substituents and poly-3-hydroxyvaleric acid (hereinafter, sometimes abbreviated

as PHV). It is known that the synthetic route of PHAs aimed at in the present invention is an independent

10 route from the synthetic route producing PHB and PHV,

and Japanese Patent Application Laid-Open No. 5-49487

did not refer to the effect of yeast extract in the synthetic route of PHAs aimed at in the present

invention at all. Further, for the effect of yeast

15 extract, it is indicated only that addition of yeast extract has a promoting effect on increasing

accumulated amount of PHAs in the bacterial body, and

it is specified that yeast extract is added not aiming at multiplication.

20 In the present invention, production/accumulation of PHA as well as multiplication is performed by making a substituted benzoylalkanoic acid coexist with yeast

extract, the yeast extract showing a quite different

effect. Further, the above inventions neither refer to

25 the prioritization of a specified monomer unit at all

which is an effect of the present invention nor show

the effect of prioritization of the specified monomer



unit which has a substituted benzoyl group as a substituent as the present invention does.

Further, examples in which yeast extract is used for production of PHAs by microorganisms include a method using *Pseudomonas putida* described in Japanese Patent Publication No. 2989175. The method of producing PHAs disclosed here is only that by 2-step culture and it is disclosed that accumulation of PHA is performed only in the 2nd step of culture under the limitation of nutrition sources except for a carbon source. In this point, the above described method is quite different in composition and effect from that of the present invention in which desired PHAs are synthesized/accumulated through only 1 step culture with the medium containing a substituted benzoylalkanoic acid and yeast extract.

Furthermore, the effect of yeast extract in Japanese Patent No. 2989175 aims at, in the 1st step of culture, only growth of the microorganisms to be used for the 2nd step of culture when using 2-step culture and it is specified that culture at the 1st step is performed under the conditions rich in nutrition sources. Herein, the substrate of PHA does not coexist at the 1st step, whereas the effect of yeast extract in the present invention is to carry out production/accumulation of PHA by making a substituted benzoylalkanoic acid coexist with yeast extract as well

as multiplication, the yeast extract showing a quite different effect.

Furthermore, in Japanese Patent No. 2989175, any of citric acid, octanoic acid and nonanoic acid coexists as a carbon source at the 1st step of culture, therefore the above method is different also in composition from the present invention in which only a substituted benzoylalkanoic acid coexists with yeast extract.

10 <Polypeptone: difference from prior arts>

One of the methods for manufacturing PHAs of the present invention is characterized in that the content rate of intended monomer units is markedly increased or only the intended monomer units exist in PHAs produced/accumulated by microorganisms by adding only polypeptone as a carbon source besides the alkanolic acid in addition to the alkanolic acid for introducing desired monomer units into the medium when culturing the microorganisms. This promoting effect of prioritizing the specific monomer unit is obtained by addition of only polypeptone as a carbon source besides the alkanolic acid to the medium.

For examples using polypeptone for PHA production by microorganisms, Japanese Patent Application Laid-Open No. 5-49487, Japanese Patent Application Laid-Open No. 5-64591, Japanese Patent Application Laid-Open No. 5-214081, Japanese Patent Application Laid-Open

No. 6-145311, Japanese Patent Application Laid-Open  
No. 6-284892, Japanese Patent Application Laid-Open  
No. 7-48438, Japanese Patent Application Laid-Open  
No. 8-89264, Japanese Patent Application Laid-Open  
5 No. 9-191893, Japanese Patent Application Laid-Open  
No. 11-32789 and so on disclose that the medium is made  
to contain polypeptone when PHAs are produced by  
microorganisms, however, in any of the above described  
patents, polypeptone is used in the pre-culture step,  
10 i.e. it is used in only the step of proliferation of  
bacteria, and the substrate to be the monomer unit of  
PHA is not contained when pre-culturing. There are  
also no examples where polypeptone is used in the step  
of producing PHAs by bacteria.

15 In contrast, in the present invention, production  
and accumulation of PHAs are performed by making an  
alkanoic acid for introducing desired monomer units  
coexist with only polypeptone as a carbon source  
besides the present alkanoic acid as well as  
20 multiplication, the method is thus quite different in  
composition and effect from the conventional examples  
using polypeptone. Further, the above described  
patents neither refer to the prioritization of a  
specified monomer unit at all which is an effect of the  
25 present invention nor show the effect of prioritization  
of the specified monomer unit which has a substituted  
benzoyl group as a substituent.

The microorganisms and culturing steps and the like used in the present invention will be described as follows.

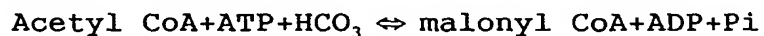
<System for supplying PHA monomer unit>

5 First, "fatty acid de novo biosynthesis", one of systems supplying the mcl-3HA monomer unit which will be mixed into the targeting PHA will be described in detail.

10 When a saccharide such as glucose is used as a substrate, an alkanolic acid necessary as a cell component is biosynthesized through the "fatty acid de novo biosynthesis" with acetyl CoA as a starting material which is produced via "glycolysis system" from saccharides. The biosynthetic pathway of fatty acid  
15 includes the de novo synthetic pathway and carbon chain-elongating pathway which will be described as follows.

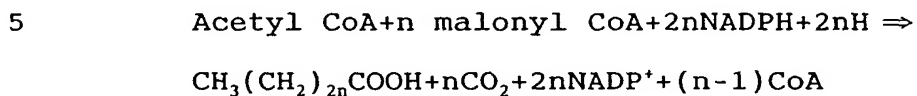
(1) De novo synthetic pathway

This is catalyzed by two enzymes which are acetyl  
20 CoA carboxylase (EC 6.4.1.2) and synthetic enzyme of fatty acid (EC 2.3.1.85). The acetyl CoA carboxylase is an enzyme which finally catalyzes the following reaction mediated by biotin and generates malonyl CoA from acetyl CoA, and the reaction is represented as the  
25 following formula:

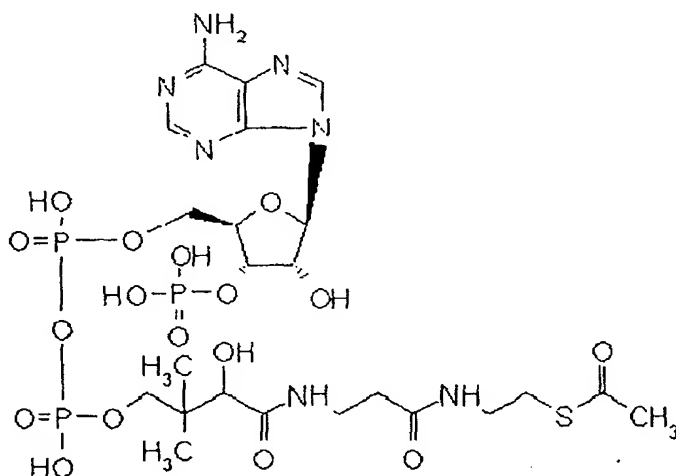


The synthetic enzyme of fatty acid is an enzyme

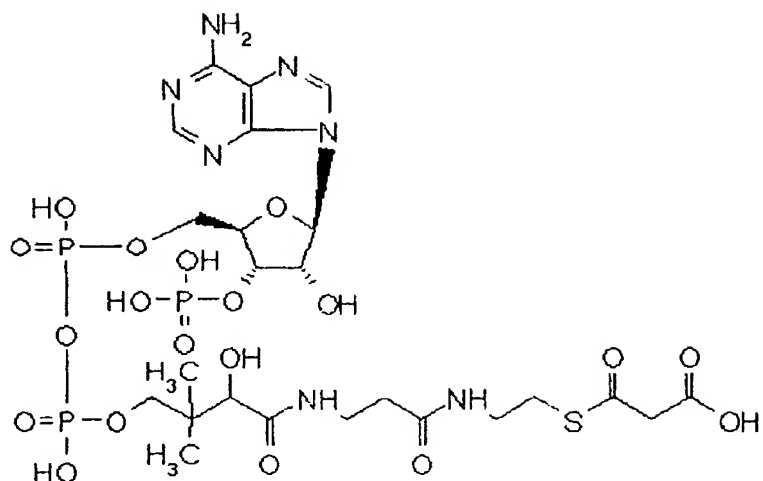
which catalyzes the reaction cycle of transition-  
condensation-reduction-dehydration-reduction, and the  
whole reactions are represented as the following  
formula:



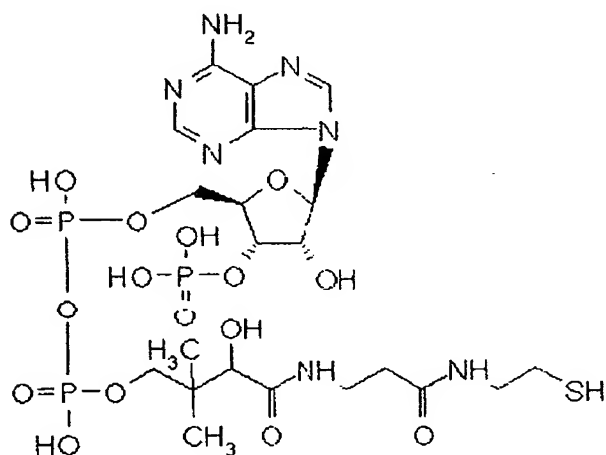
              In addition, reaction products will be free acids,  
CoA derivatives or ACP derivatives depending on the  
type of enzyme. Herein, the acetyl CoA is represented  
10 as the following chemical formula.



Malonyl CoA is represented by the following  
chemical formula.

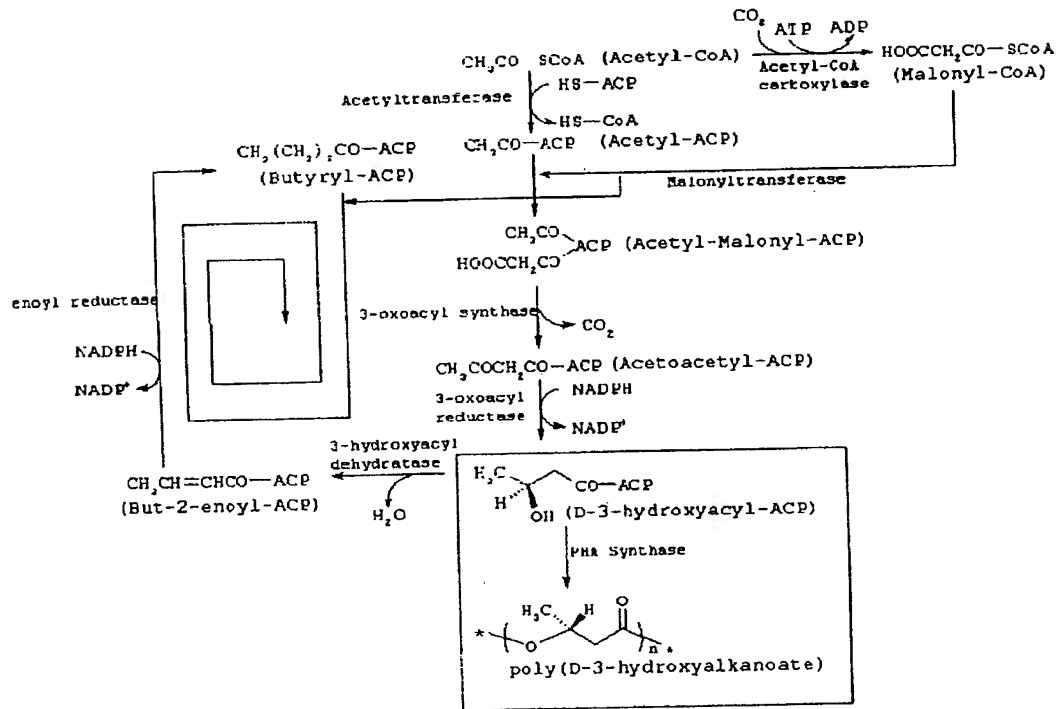


Herein, CoA is the abbreviated name for coenzyme A which is represented by the following chemical formula.



Of the present reaction pathways, "D-3-hydroxyacyl ACP" which will be a monomer substrate of PHA biosynthesis is supplied as an intermediate through the pathway as shown below. In addition, adding two carbons each through the pathway as shown in the following reaction scheme, finally it is extended to palmitic acid. Therefore, as a monomer substrate of the PHA biosynthesis, seven "D-3-hydroxyacyl ACPs" of

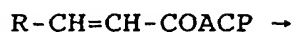
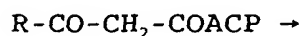
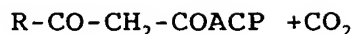
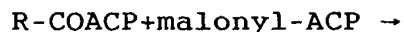
"D-3-hydroxybutyryl ACP" to "D-3-hydroxypalmityl ACP"  
will be supplied where the number of carbons is even.



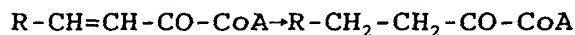
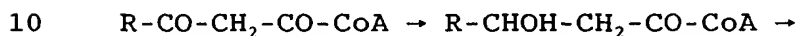
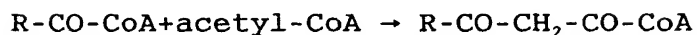
## (2) Pathway of carbon chain elongation

These pathways are roughly divided into two pathways including the pathway (designated as Pathway A) where malonyl ACP is added to acyl ACP finally becoming acyl ACP (and  $\text{CO}_2$ ) elongated by two carbon chains and the pathway (designated as Pathway B) where acetyl CoA is added to acyl CoA finally becoming acyl CoA elongated by two carbon chains. Each pathway will be described as follows.

. Pathway A



. Pathway B



Both A and B pathways generate "D-3-hydroxyacyl CoA" or "D-3-hydroxyacyl ACP" as an intermediate, and it is considered that "D-3-hydroxyacyl CoA" itself is  
 15 utilized as a monomer substrate of the PHA biosynthesis and "D-3-hydroxyacyl ACP" is utilized as a monomer substrate of the PHA biosynthesis after it is converted into "D-3-hydroxyacyl CoA" by ACP-CoA transferase.

When using saccharides such glucose as a  
 20 substrate, it is considered that a mcl-3HA monomer unit is produced through "glycolysis system" and "biosynthetic pathway of fatty acid". Further, when using an organic acid involved in the TCA cycle as a substrate, the acetyl CoA is directly produced from  
 25 pyruvic acid by pyruvate dehydrogenase. Phosphoenolpyruvic acid is generated from oxaloacetic acid by phosphoenolpyruvate carboxynase which is then



catalyzed by pyruvate kinase to generate pyruvic acid,  
further generating by acetyl CoA through the above  
reaction. It is considered that the acetyl CoA  
generated by these reactions produces the mcl-3HA  
5 monomer unit through "biosynthetic pathway of fatty  
acid".

Herein, it is considered that e.g. mcl-alkanoic  
acid such as octanoic acid and nonanoic acid or e.g.  
alkanoic acid in which a functional group other than a  
10 straight chain aliphatic alkyl is added at the end,  
e.g. 5-phenylvaleric acid, 4-phenoxybutyric acid 4-  
cyclohexylbutyric acid are converted into CoA  
derivatives by CoA ligase (EC 6.2.1.3 etc.) and  
directly into "D-3-hydroxyacyl CoA" which will be a  
15 monomer substrate of the PHA biosynthesis by an enzyme  
group carrying  $\beta$ -oxidation system.

In short, while a mcl-3HA monomer unit generated  
from saccharides or an organic acid involved in the TCA  
cycle is produced through extremely multi-step enzyme  
20 reactions (i.e. indirectly), the mcl-3HA monomer unit  
from mcl-alkanoic acid will be produced very directly.

Here, generation of acetyl CoA in charge of growth  
of microorganisms will be described. In a method where  
a mcl-alkanoic acid is made to coexist in addition to  
25 an alkanoic acid for introduction of an intended  
monomer unit, acetyl CoA is generated from these  
alkanoic acids through the  $\beta$ -oxidation system.

Comparing with alkanolic acids having bulky substituents (alkanoic acids having substituents such as a phenyl group, a phenoxy group, a cyclohexyl group or the like), the mcl-alkanoic acid is generally considered to  
5 be excellent in substrate affinity to an enzyme group in the  $\beta$ -oxidation system, and the acetyl CoA is effectively produced by coexistence of the mcl-alkanoic acid. Therefore, this is advantageous for growth of microorganisms where the acetyl CoA is used as an  
10 energy source and a carbon source.

However, since the mcl-alkanoic acid through the  $\beta$ -oxidation system is directly converted into a PHA monomer unit, it is a big problem that the PHA produced comprises a large amount of a mcl-3HA monomer unit in  
15 addition to an intended monomer unit.

In order to solve this problem, a desirable method is that a substrate other than the mcl-alkanoic acid which may supply effectively acetyl CoA or an energy source and a carbon source is selected and made to  
20 coexist with an intended alkanolic acid. As aforementioned, while the acetyl CoA may be converted into a PHA monomer unit through the biosynthetic pathway of fatty acid, this is indirect and requires passing through more multi-step reactions comparing  
25 with the mcl-alkanoic acid. By selecting appropriate culture conditions including concentration of the substrate which may generate acetyl CoA, a

manufacturing method substantially without or with less mixing of mcl-3HA is feasible.

A manufacturing method where a microorganism is cultured aiming at only its growth in the first step and subsequently in the second step only an intended alkanoic acid as a carbon source is added into the culture medium is widely used. Herein, acyl CoA ligase which is an initiating enzyme in the  $\beta$ -oxidation system converting the alkanoic acid to the acyl CoA requires ATP, and according to the present inventors' investigation, by obtaining the results that a manufacturing method where a substrate which a microorganism can use as an energy is made to coexist also in the second step is more effective, the present invention was completed.

For a substrate which can supply effectively acetyl CoA or an energy source and a carbon source in the present inventive method, any compounds may be used including: aldoses such as glyceroaldehyde, erythrol, arabinose, xylose, glucose, galactose, mannose and fructose; alditols such as glycerol, erythritol and xylitol; aldonic acids such as gluconic acid; uronic acids such as glucuronic acid and galacturonic acid; saccharides such as disaccharides e.g. maltose, sucrose and lactose; and organic acids involved in the TCA cycle such as lactic acid, pyruvic acid, malic acid, citric acid, succinic acid, fumaric acid, and their

salts; further natural culture component such as yeast extract, polypeptone, meat extract, casamino acid and the like, if they can supply the acetyl CoA or the energy source and carbon source without passing through the  $\beta$ -oxidation system, and they can be suitably selected for usefulness as a substrate to a strain used. Further, if the combination has less mixture of mcl-3HA, it is possible to select plural compounds to be used.

10 <Microorganism>

Microorganisms used in the present invention, any of them may be used if they can produce PHA comprising the above described 3-hydroxy-substituted-benzoylalkanoic acid unit using the above described substituted benzoylalkanoic acid as a material. Further, in the scope of attaining the present inventive purposes, plural microorganisms may be mixed to be used if necessary.

Using FBzVA etc. as a substrate, the present inventors searched microorganisms which have capability of producing PHA containing the above described 3HFBzV etc. as a monomer unit and accumulating it in the bacterial body. Consequently, the present inventors have found that microorganisms, *Pseudomonas cichorii* H45 strain, *Pseudomonas cichorii* YN2 strain, *Pseudomonas jessenii* Pl61 strain, etc. isolated from soil and having capability of producing PHA had the

desired capability. Herein, these strains have been deposited in International Patent Organism Depository of General Research Institute, Independent

5 Administrative Center of Research Institute of Life Engineering, Ministry of Economy and Industry) as Deposit No. "FERM BP-7374" for the H45 strain, Deposit No. "FERM BP-7375" for the YN2 strain and Deposit No. "FERM BP-7376" for the P161 strain, respectively.

10 The bacteriological properties of the above described H45 strain, YN2 strain and P161 strain are listed as follows. In addition, for the P161 strain, the base sequence of 16sr RNA is shown in the sequence No. 1.

15 <Bacteriological property of H45 strain>  
(1) Morphological properties

Shape and size of cell: Bacillus, 0.8  $\mu\text{m}$  x 1.0-1.2  $\mu\text{m}$

Polymorphism of cell: absence

Mobility: presence

20 Spore formation: absence

Gram stainability: negative

Colony shape: round, all smooth rims, low convex, smooth surface layer, gloss and cream color

(2) Physiological properties

25 Catalase: positive

Oxidase: positive

O/F test: oxidation type

- Reduction of nitrate: negative  
Production of indole: positive  
Acidification of glucose: negative  
Arginine dihydrolase: negative
- 5 Urease: negative  
Hydrolysis of esculin: negative  
Hydrolysis of gelatin: negative  
 $\beta$ -Galactosidase: negative  
Production of fluorochrome on King's B agar: positive
- 10 Growth in 4% NaCl: negative  
Accumulation of poly- $\beta$ -hydroxybutyric acid: negative  
(3) Assimilability of substrate  
Glucose: positive  
L-Arabinose: negative
- 15 D-Mannose: positive  
D-Mannitol: positive  
N-Acetyl-D-glucosamine: positive  
Maltose: negative  
Potassium gluconate: positive
- 20 n-Caprylic acid: positive  
Adipic acid: negative  
dl-Malic acid: positive  
Sodium citrate: positive  
Phenyl acetate: positive
- 25 <Bacteriological properties of YN2 strain>  
(1) Morphological properties  
Shape and size of cell: Bacillus, 0.8  $\mu\text{m}$   $\times$  1.5-2.0  $\mu\text{m}$

Polymorphism of cell: absence

Mobility: presence

Spore formation: absence

Gram stainability: negative

- 5 Colony shape: round, all smooth rims, low convex,  
smooth surface layer, gloss, cream color and  
translucent

(2) Physiological properties

Catalase: positive

- 10 Oxidase: positive

O/F test: oxidation type

Reduction of nitrate: negative

Production of indole: positive

Acidification of glucose: negative

- 15 Arginine dihydrolase: negative

Urease: negative

Hydrolysis of esculin: negative

Hydrolysis of gelatin: negative

$\beta$ -Galactosidase: negative

- 20 Production of fluorochrome on King's B agar: positive

Growth in 4% NaCl: positive (weak growth)

Accumulation of poly- $\beta$ -hydroxybutyric acid: negative

Hydrolysis of Tween 80: positive

(3) Assimilability of substrate

- 25 Glucose: positive

L-Arabinose: positive

D-Mannose: negative

- D-Mannitol: negative  
N-Acetyl-D-glucosamine: negative  
Maltose: negative  
Potassium gluconate: positive
- 5 n-Caprylic acid: positive  
Adipic acid: negative  
dl-Malic acid: positive  
Sodium citrate: positive  
Phenyl acetate: positive
- 10 <Bacteriological properties of P161>  
(1) Morphological properties  
Shape and size of cell: sphere,  $\phi$  0.6  $\mu\text{m}$   
Bacillus, 0.6  $\mu\text{m}$   $\times$  1.5-2.0  $\mu\text{m}$   
Polymorphism of cell: presence (elongation type)
- 15 Mobility: presence  
Spore formation: absence  
Gram stainability: negative  
Colony shape: round, all smooth rims, low convex,  
smooth surface layer, gloss and pale yellow
- 20 (2) Physiological properties  
Catalase: positive  
Oxidase: positive  
O/F test: oxidation type  
Reduction of nitrate: positive
- 25 Production of indole: negative  
Acidification of glucose: negative  
Arginine dihydrolase: positive



Urease: negative

Hydrolysis of esculin: negative

Hydrolysis of gelatin: negative

$\beta$ -Galactosidase: negative

5 Production of fluorochrome on King's B agar: positive

(3) Assimilability of substrate

Glucose: positive

L-Arabinose: positive

D-Mannose: positive

10 D-Mannitol: positive

N-Acetyl-D-glucosamine: positive

Maltose: negative

Potassium gluconate: positive

n-Caprylic acid: positive

15 Adipic acid: negative

dl-Malic acid: positive

Sodium citrate: positive

Phenyl acetate: positive

In addition to *Pseudomonas* genus, it is possible  
20 to use microorganisms which belong to *Aeromonas* sp.,  
*Comamonas* sp. or *Burkholderia* sp. and produce PHA  
comprising the above described 3-hydroxy-substituted  
benzoylalkanoic acid unit as a monomer unit using the  
above substituted benzoylalkanes as a material.

25 <Culture>

The intended PHA can be produced by culturing  
these microorganisms in a culture medium containing an

alkanoic acid for introduction of a desired monomer unit and a substrate for growth of the present invention. Such a PHA is generally composed of only the R-configuration being an isotactic polymer.

5           For the usual culture of the microorganism used in the manufacturing method of PHA relating to the present invention, for example, preparation of stored strains and growth for retaining bacterial count and active condition required for production of PHA and the like,  
10   the culture medium containing components required for growth of microorganisms used is suitably selected to be used. For example, any types of culture medium such as the general natural one (meat extract, yeast extract or the like) or the synthetic one with nutrients added  
15   can be used so long as they do not have a bad influence on growth and survival of microorganisms.

          Any culture methods such as liquid culture and solid culture may be used if they can multiply the microorganisms and produce PHA. Further, any types of  
20   culture can be used without regard to batch culture, fed batch culture, semi-continuous culture, continuous culture or the like. As a form of the liquid batch culture, there are methods of supplying oxygen by shaking using a shaking flask and by a stirring  
25   aeration method using a jar fermenter. A multi-step method in which a plurality of these steps are connected may be adopted.

When manufacturing PHAs comprising 3-hydroxy-substituted benzoylalkanoic acid units using PHA-producing microorganisms as described above, an inorganic medium etc. containing at least respective corresponding substituted  
5 benzoylalkanoic acids as materials for PHA production and a carbon source for growth of microorganisms can be used.

As the carbon source for growth, it is possible to use the medium components originated in natural products such as yeast extract, polypeptone, meat extract, casamino acid and  
10 the like, further any compounds such as saccharides, organic acids involved in the Tlc cycle (organic acids generated as intermediates in the TCA cycle and those generated through one or two steps of biochemical reactions from the TCA cycle) or their salts or the like can be used if they  
15 generate acetyl CoA without passing through the  $\beta$ -oxidation cycle, and can be suitably selected for usefulness as a substrate to a used strain. In addition, it is possible to select plural compounds to be used if the combination has less mixture of mcl-3HA.

20 Of them, for saccharides, one or more compounds selected from aldoses such as glyceroaldehyde, erythrose, arabinose, xylose, glucose, galactose, mannose or fructose; alditols such as glycerol, erythritol or xylitol; aldonic acids such as gluconic acid; uronic acids such as glucuronic acid or

galacturonic acid; disaccharides such as maltose, sucrose or lactose can be suitably used.

Examples of organic acids or their salts include pyruvic acid, oxaloacetic acid, citric acid, isocitric acid, ketoglutaric acid, succinic acid, fumaric acid, malic acid or lactic acid, or one or more compounds selected from their salts can be suitably used. Of them, particularly use of saccharides is preferable, particularly at least one selected from a group consisting of glucose, fluctose and mannose is more preferable.

For the method for producing /accumulating PHAs by microorganisms, the productivity sometimes improves when sufficient multiplication is performed first, then the bacteria are transferred into the medium with a limited nitrogen source such as ammonium chloride and further cultured in the state with a compound added as a substrate of an intended unit. Specifically, adoption of multi-step method in which a plurality of the above described steps are connected is included. For example, there is a method where culturing is performed in the inorganic medium etc. containing about 0.05% to 5.0% of D-glucose and about 0.01% to 1.0% of a substituted benzoylalkanoic acid from the logarithmic growth up to the stationary phase the bacteria are recovered by centrifugal separation etc., and further they are cultured in an inorganic medium containing

about 0.01% to 1.0% of the substituted benzoylalkanoic acid with a limited nitrogen source or without its existence substantially.

For the inorganic medium used in the above culturing method, any types if they contain components such as a phosphorous source (e.g. phosphate etc.), a nitrogen source (e.g. ammonium salt, nitrate, etc.) and the like capable of growing microorganisms may be used, for example, the inorganic salt medium may include the MSB medium, E medium (J. Biol. Chem., 218, 97-106 (1956)), M9 medium and the like. Herein, composition of the M9 medium used in Examples of the present invention is as follows.

$\text{Na}_2\text{HPO}_4$ : 6.2 g

$\text{KH}_2\text{PO}_4$ : 3.0 g

15  $\text{NaCl}$ : 0.5 g

$\text{NH}_4\text{Cl}$ : 1.0 g

(in 1 liter of the medium, pH 7.0)

Further, in order to perform good growth and production of PHA, it is preferable to add about 0.3% (v/v) of a solution of the following trace components into the above inorganic salt medium.

Trace component solution

Nitrilotriacetic acid: 1.5 g

$\text{MgSO}_4$ : 3.0 g

25  $\text{MnSO}_4$ : 0.5 g

$\text{NaCl}$ : 1.0 g

$\text{FeSO}_4$ : 0.1 g

CaCl<sub>2</sub>: 0.1 g

CoCl<sub>2</sub>: 0.1 g

ZnSO<sub>4</sub>: 0.1 g

CuSO<sub>4</sub>: 0.1 g

5 AlK(SO<sub>4</sub>)<sub>2</sub>: 0.1 g

H<sub>3</sub>BO<sub>3</sub>: 0.1 g

Na<sub>2</sub>MoO<sub>4</sub>: 0.1 g

NiCl<sub>2</sub>: 0.1 g

(in 1 liter)

10 For the culturing temperature, any temperature may be used if it enables the above described strains to grow well for example, 15-40°C, preferably 20-35°C and more preferably about 20-30°C are appropriate.

As a specific example, culturing is performed in the  
15 inorganic medium etc. containing about 0.05% to 5.0% of D-glucose and about 0.01% to 1.0% of a substituted benzoylalkanoic acid, the bacterial bodies were at the time from the logarithmic growth phase up to the stationary phase, the desired PHA with less mixture of unintended monomer units  
20 or without them at all can be extracted. Such PHA is generally composed of only the R-configuration being isotactic polymer.

The same amount of an organic acid involved in the TCA cycle, yeast extract and polypeptone instead of D-glucose may  
25 be added and their combination may be used.

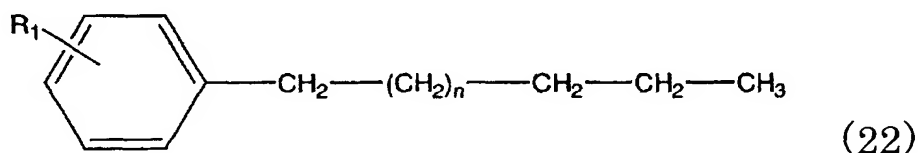
<Recovery of PHA>

For obtaining PHA from the culture solution relating to the present invention, the methods performed usually are applicable. When PHA is discharged in the culture solution, methods of extraction and purification from the culture solution are used and when PHA is accumulated in the bacterial bodies, methods of extraction and purification from bacterial bodies are used. For recovery of PHA from the cultured bacterial body of microorganism, for example, while extraction with organic solvents such as chloroform performed usually is the simplest, dioxane, tetrahydrofuran, acetonitrile and acetone besides chloroform are sometimes used. In the circumstance difficult to use organic solvents, the following methods also can be used: the bacterial body components except PHA are removed by fracturing the microorganism cells physically using any methods of treatment with a surfactant such as SDS, treatment with an enzyme such as lysozyme, treatment with agents such as EDTA, hydrogen peroxide, sodium hypochlorite and ammonia, or the ultrasonic fracturing method, homogenizer method, pressure fracturing method, beads impact method, grinding method, mashing method and freeze-thaw method to recover PHA.

In addition, culturing of microorganisms by the present invention, production of PHAs and their accumulation into the bacterial body by microorganisms

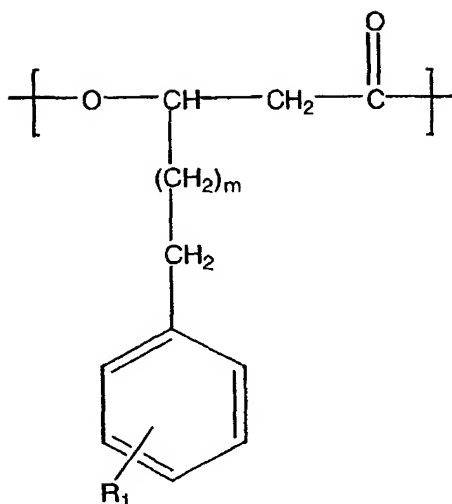
of the present invention and recovery of PHAs from the bacterial body of the present invention are not limited to the above described methods.

The second example of compounds used as starting materials in the present invention can include at least one selected from substituted phenylalkanes represented by the chemical formula (22), and polyhydroxyalkanoates manufactured in that case can include polyhydroxyalkanoates containing at least one selected from 3-hydroxy(substituted phenyl)alkanoate units represented by the chemical formula (23) in the molecule:



wherein  $R_1$  shows a substituent on the aromatic ring and is at least one selected from an H atom, a CN group, an  $NO_2$  group, a halogen atom, a  $CH_3$  group, a  $C_2H_5$  group, a  $C_3H_7$  group, a  $CH_2=CH$  group, a  $CF_3$  group, a  $C_2F_5$  group and a  $C_3F_7$  group; and  $n$  is an optional integer selected from 0 to 9), and

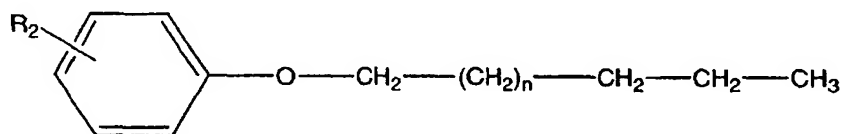




(23)

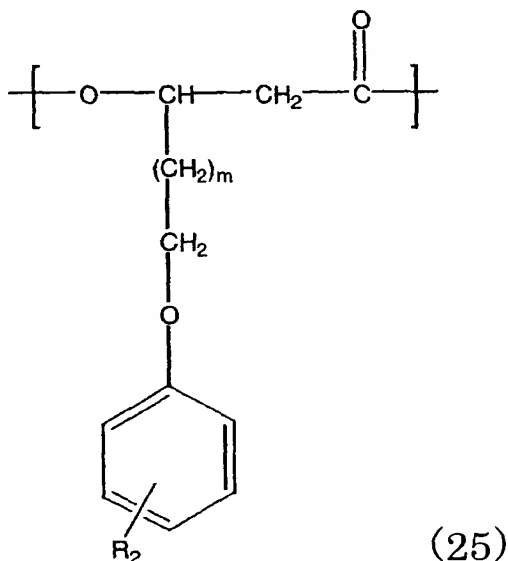
wherein  $R_1$  shows a substituent on the aromatic ring and is at least one selected from an H atom, a CN group, an  $\text{NO}_2$  group, a halogen atom, a  $\text{CH}_3$  group, a  $\text{C}_2\text{H}_5$  group, a  $\text{C}_3\text{H}_7$  group, a  $\text{CH}_2=\text{CH}$  group, a  $\text{CF}_3$  group, a  $\text{C}_2\text{F}_5$  group and a  $\text{C}_3\text{F}_7$  group; and  $m$  is an optional integer selected from 0 to 9.

The second example of compounds used as starting materials in the present invention can include at least one selected from substituted phenoxyalkanes represented by the chemical formula (24), polyhydroxyalkanoates manufactured in that case can include those containing at least one in the molecule selected from 3-hydroxy(substituted phenoxy)alkanoate units represented by the chemical formula (25):



(24)

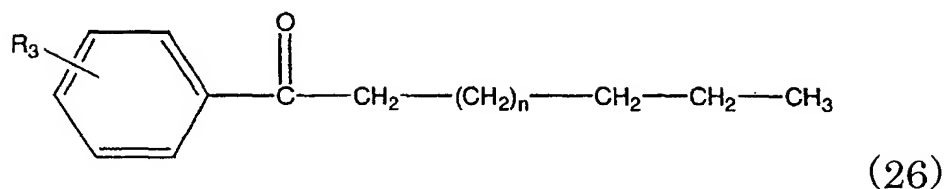
wherein  $R_2$  shows a substituent on the aromatic ring and is at least one selected from an H atom, a CN group, an  $NO_2$  group, a halogen atom, a  $CH_3$  group, a  $C_2H_5$  group, a  $C_3H_7$  group, a  $CF_3$  group, a  $C_2F_5$  group and a  $C_3F_7$  group; and n is an optional integer selected from 0 to 9, and



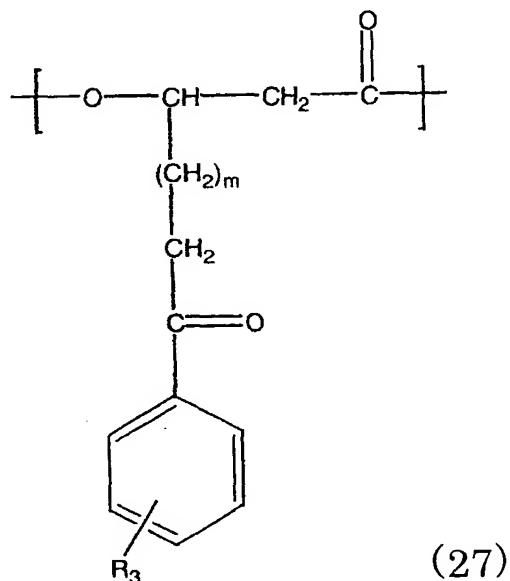
wherein  $R_2$  shows a substituent on the aromatic ring and is at least one selected from an H atom, a CN group, an  $NO_2$  group, a halogen atom, a  $CH_3$  group, a  $C_2H_5$  group, a  $C_3H_7$  group, a  $CF_3$  group, a  $C_2F_5$  group and a  $C_3F_7$  group; and m is an optional integer selected from 0 to 9.

The third example of compounds used as starting materials in the present invention can include at least one selected from substituted benzoylalkanes represented by the chemical formula (26), polyhydroxyalkanoates manufactured in that case can include those containing at least one in the molecule selected from 3-hydroxy(substituted benzoyl)alkanoate

units represented by the chemical formula (27):



wherein  $\text{R}_3$  shows a substituent on the aromatic ring and is at least one selected from an H atom, a CN group, an  $\text{NO}_2$  group, a halogen atom, a  $\text{CH}_3$  group, a  $\text{C}_2\text{H}_5$  group, a  $\text{C}_3\text{H}_7$  group, a  $\text{CF}_3$  group, a  $\text{C}_2\text{F}_5$  group and a  $\text{C}_3\text{F}_7$  group; and  $n$  is an optional integer selected from 0 to 9, and



wherein  $\text{R}_3$  shows a substituent on the aromatic ring and is at least one selected from an H atom, a CN group, an  $\text{NO}_2$  group, a halogen atom, a  $\text{CH}_3$  group, a  $\text{C}_2\text{H}_5$  group, a  $\text{C}_3\text{H}_7$  group, a  $\text{CF}_3$  group, a  $\text{C}_2\text{F}_5$  group and a  $\text{C}_3\text{F}_7$  group; and  $m$  is an optional integer selected from 0 to 9

Describing the present inventive method more

specifically, the manufacturing method of polyhydroxyalkanoates comprising one or more 3-hydroxyalkanoic acid units represented by the above described chemical formulas (23), (25) and (27)

5 contains the processes where microorganisms are cultured in the medium containing one or more of any compounds represented by the above described chemical formulas (22), (24) and (26).

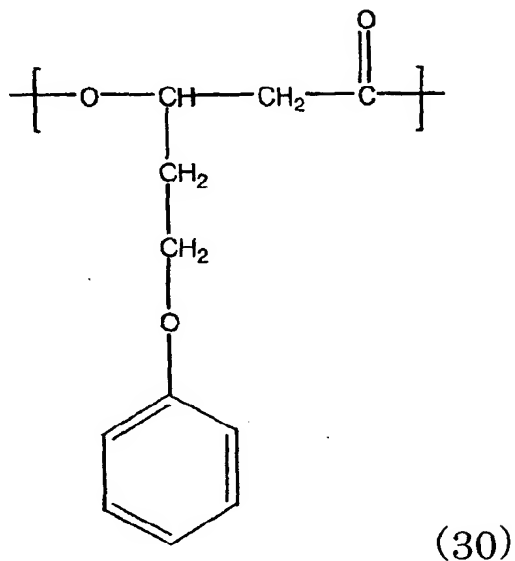
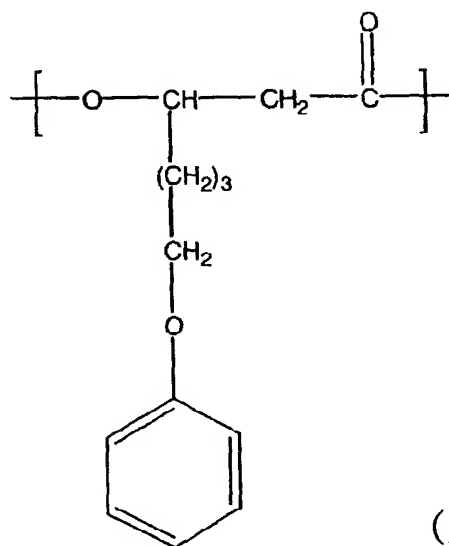
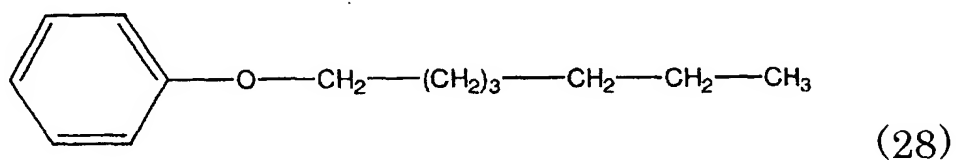
Thus, in the manufacturing method of the present invention, when comprising a step of culturing a microorganism, i.e. a producing step of the polyhydroxyalkanoates by the microorganism, relationship between methylene chain length "n" showing in the formula of the starting material represented by the above described chemical formulas (22), (24) and (26) and side chain methylene chain length "m" shown in the formula represented by the above described chemical formulas (23), (25) and (27) of the units present in the molecules of the polyhydroxyalkanoates manufactured by the present inventive method can be designated as the following equation (1):

$$m=n-2l \quad (1)$$

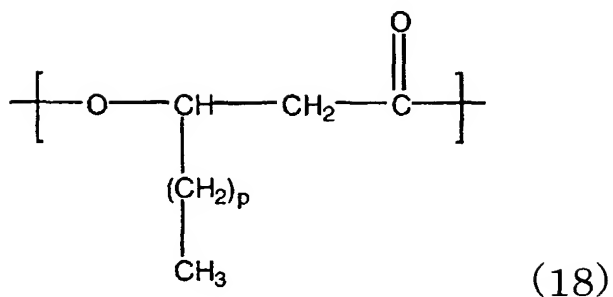
wherein  $l$  is an optional integer of  $0 \leq l < (1/2)n$

For example, when using 7-phenoxyheptane represented by the chemical formula (28) as a starting material, the polyhydroxyalkanoate produced comprises a 3-hydroxy-7-phenoxyheptanoic acid unit represented by

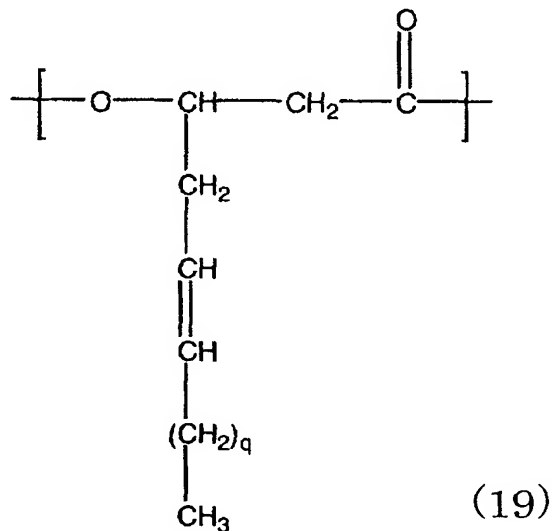
the chemical formula (29) and a 3-hydroxy-5-phenoxyvaleric acid unit represented by the chemical formula (30):



Further, the PHA obtained by the present inventive method may comprise at least one of units contained in the polymer molecule, which are a 3-hydroxyalkanoic acid unit represented by the following general formula (18):



wherein p is an optional integer selected from 0 to 8 which can take one or more values in the polymer or a 3-hydroxy-alka-5-enoic acid unit represented by the following formula (19):



wherein z is an optional integer selected from 3 or 5 which can take one or more values in the polymer.

Furthermore, the number average molecular weight of PHAs obtained in the present inventive method is about 5000 to 1000000.

Microorganisms, culturing step, recovering step, etc. utilized in the present invention will be

described as follows.

(Microorganisms)

Microorganisms used in the present inventive method can use any of them if polyhydroxyalkanoates containing a 3-hydroxy-substituted alkanoate unit in the molecule shown in general formula (14) having residues comprising substituted aromatic rings as shown in chemical formulas (15), (16) and (17) at the side chain can be produced using substituted alkanes of starting compounds as substrate materials shown in general formula (13) having residues comprising substituted aromatic rings as shown in chemical formulas (15), (16) and (17). Further, plural microorganisms can be mixed to be used within the scope that can attain the present inventive purposes if necessary.

Microorganisms used in the present invention are required to have at least capability of converting an alkane to an alkanoic acid, further they have capability of producing the PHA from the alkanoic acid. The capability of converting the alkane to the alkanoic acid is usually exhibited by having a group of enzymatic systems with alkane monooxygenase as a starting enzyme.

For such microorganisms, the microorganisms which belong to Pseudomonas genus are known, more specifically they are microorganisms separated from

soil including *Pseudomonas cichorii* YN2 strain disclosed in Japanese Patent Application No. 11-371863 and *Pseudomonas oleovorans* ATCC 29347 disclosed in Japanese Patent Application Laid-Open No. 63-226291.

5           (Culturing step)

          In the culturing step of the manufacturing method of PHA s relating to the present invention, a polyhydroxyalkanoate which comprises at least one selected from a 3-hydroxy-substituted alkanoate unit  
10       group represented by the above described general formula (14) in the molecule is produced from at least one selected from a corresponding substituted alkane group represented as general formula (13) as a starting material using the above described microorganisms  
15       capable of producing the polyhydroxyalkanoate.

          For usual culture of microorganisms used in this culturing step, e.g. preparation of the stored bacterial strain, multiplication to ensure the bacteria count or their active state required for production of  
20       PHA etc., the medium which contains the components required for growth of microorganisms used is suitably selected to be used. For example, any type of medium such as typical natural mediums (meat extract medium, yeast extract, etc.) and synthetic mediums with  
25       nutrition sources added may be used. Culturing conditions including temperature, aeration and agitation are suitably selected as the microorganisms



used demand.

On the other hand, in the culturing step, when manufacturing the PHA which comprises at least one selected from an intended 3-hydroxy-substituted-  
5 alkananoate unit group represented as general formula (14) in the molecule using the above described PHA-producing microorganisms, the inorganic medium and the like which contain at least a carbon source for growth of microorganisms in addition to one selected from the  
10 group of substituted alkanes represented as the above described general formula (13) corresponding to the monomer unit as a material for the PHA production may be used as a medium. The initial content rate of the group of substituted alkanes represented as general  
15 formula (13) as a material is preferably selected with in the range of 0.01%-1% (v/v) per medium, more preferably 0.02%-0.2% (v/v).

The culturing step of the manufacturing method may be comprised of a step for culturing the microorganism in a medium containing dicyclopropylketone which induces alkane oxidation pathway. In general, linear  
5 alkane which is the substrate in a metabolic pathway of the alkane oxidation pathway, like octane and nonane, induces alkane oxidation pathway effectively. However, when such a linear alkane is used as an inducer, obtained PHA has high composition ratio of the medium-  
10 chain-length 3-hydroxyalkanoate units. Because linear

alkane is converted to linear alkanoic acid through alkane oxidation pathway, and subsequently converted to a monomer substrate of the PHA through  $\beta$ -oxidation pathway.

5           The substituted alkanes used for monomer substrates in the present invention can also induce alkane oxidation pathway, therefore they can be incorporated as monomer units of PHA like the above-mentioned linear alkane. Alkane oxidation pathway has  
10 evolved to adapt linear alkane, consequently the substituted alkanes of the invention may not induce the pathway sufficiently compared with linear alkanes.

          Dicyclopentylketone is known as gratuitous inducer. It functions as an inducer for the alkane  
15 oxidation pathway. However it cannot be oxidized by alkanemonooxygenase, hence it does not function as a substrate of the pathway (Journal of Bacteriology, 123, 546-556 (1975)). On this account, when induction of the alkane oxidation pathway is insufficient or to be  
20 enhanced, or target PHA needs a low composition ratio of medium-chain-length 3-hydroxyalkanoate units, dicyclopentylketone can be used for preferable inducer. In this case, dicyclopentylketone induces alkane  
25 oxidation pathway effectively and whole metabolizing activity can be used for the conversion of the substituted alkanes of the present invention. As a result, monomer units derived from the substituted

alkanes are produced effectively and high yield of PHA and high composition ratio of monomer units derived from substituted alkanes are achieved.

Dicyclopropylketone only can be added to the culture medium or added with the substituted alkanes of the present invention. Concentration of the dicyclopropylketone is selected in consideration of a culture condition such as kind of nutrients in the medium, presence or absence of the substituted alkanes and their concentrations, number of the culturing steps and which step is it. The concentration of dicyclopropylketone is usually within the range of 0.001% to 1% (v/v), more preferably within the range of 0.01% to 0.1%.

The group of substituted alkanes represented by the general formula (13) does not always have good water solubility owing to its hydrophobicity, which is, however, not problematic at all because the above-described microorganisms have a characteristic of enabling to utilize this compound as a substrate and even though there is some portion over the solubility partly in the suspended state at the beginning of culturing, the microorganisms gradually take it into their cells during continuation of culture to solve it in the medium in turn. Further, it is sometimes seen that the microorganism itself secretes a surfactant-like substance for efficient uptake, therefore it

makes uptake of the substituted alkane as a substrate easy.

In addition, the group of substituted alkanes represented as general formula (13) as a material may  
5 be added to the medium sometimes in a solution of the solvent such as 1-hexadecene and n-hexadecane or in a form of fine suspension to increase its dispersibility. In such a case, the addition concentration of solvents such as 1-hexadecene and n-hexadecane used is required  
10 to be not more than 3% (v/v) to the medium.

In the medium, the substrate for growth which the microorganism utilize for its growth is added separately. For this substrate for multiplication, nutrients such as yeast extract, polypeptone and meat  
15 extract may be used. Further, they may be suitably selected from saccharides, organic acids generated as intermediates in the TCA cycle and organic acids generated through one step or two steps of biochemical reactions from the TCA cycle or their salts, amino  
20 acids or their salts, straight chain alkanoic acids having 4 to 12 carbons or their salts or the like, according to the strain used and considering their usefulness as a carbon source.

Of these various substrates for multiplication,  
25 suitably usable saccharides are one or more compounds selected from the group consisting of: aldoses such as glyceroaldehyde, erythrose, arabinose, xylose, glucose,

galactose, mannose or fluctose; alditols such as  
glycerol, erythritol or xylitol; aldonic acids such as  
gluconic acid; uronic acids such as glucuronic acid or  
galacturonic acid; disaccharides such as maltose,  
5 sucrose or lactose.

Further, suitably usable organic acids or their  
salts are one or more compounds selected from the group  
consisting of pyruvic acid, malic acid, lactic acid,  
citric acid, succinic acid or their salts. On the  
10 other hand, suitably usable amino acids or their salts  
are one or more compounds selected from the group  
consisting of glutamic acid, aspartic acid or their  
salts.

Generally, of these various substrates for  
15 multiplication, it is generally more preferable to use  
polypeptone and saccharides, and of saccharides, it is  
further preferable to use at least one selected from  
the group consisting of glucose, fluctose or mannose.  
The content ratio of these substrates for  
20 multiplication is desirably selected to be usually  
within the range of 0.1%-5% (w/v) per medium, more  
preferably within the range of 0.2%-2% (w/v).

For another method in the culturing step in which  
PHAs are produced/accumulated by a microorganism, the  
25 productivity sometimes improves when sufficient  
multiplication is performed first, then the bacteria  
are transferred into the medium with limited a nitrogen

source such as ammonium chloride and further cultured in the state with a compound added as a substrate of an intended unit. For example, adoption of the multi-step method with a plurality of steps of the above described  
5 different culture conditions connected is included.

More specifically, it is more preferable to use the two-step culturing method etc. performing;

as the first step, (step 1-1), the step of culturing a microorganism in the medium containing the  
10 group of substituted alkanes represented by the general formula (13) and polypeptone as a carbon source is continued from the logarithmic growth phase up to the stationary phase, then the bacteria are recovered by centrifugal separation once,

15 and subsequently;

as the second step, (step 1-2), the step of further culturing the microorganism cultured/multiplied in the former stage, step 1-1, in the medium containing the group of substituted alkanes represented by the  
20 general formula (13) and an organic acid or its salt as a carbon source;

as the first step, (step 1-3), the step of culturing a microorganism in the medium containing the group of substituted alkanes represented by the general  
25 formula (13) and glucose as a carbon source is continued from the logarithmic growth phase up to the stationary phase, then the bacteria are recovered by

centrifugal separation once, and subsequently;  
as the second step, (step 1-4), the step of  
further culturing the microorganism cultured/multiplied  
in the former stage, step 1-3, in the medium containing  
the group of substituted alkanes represented by the  
5 general formula (13) and glucose as a carbon source  
without a nitrogen source.

Further, it is preferable to use a two-stage  
culturing method comprising the first step (step 1-5),  
10 the step of culturing a microorganism in the medium  
containing the group of substituted alkanes represented  
by general formula (13) and polypeptone as a carbon  
source is continued up to the late logarithmic growth  
phase or the early stationary phase, then the bacteria  
15 are recovered by centrifugal separation once, and  
subsequently;

the second step (step 1-6), the step of further  
culturing the microorganism cultured in the former  
stage, step 1-5, in the medium containing the group of  
substituted alkanes represented by the general formula  
20 (13) and a saccharide as a carbon source but not  
containing any nitrogen source.

In the second step, described as (1-2), (1-4), and  
(1-6), the cultivation can be conducted without a  
25 nitrogen source.

Such two-step culturing method provides the  
following culturing forms: in the former stage, PHAs

comprising at least one selected from the group of 3-hydroxy-substituted alkanoate units represented as the above general formula (14) corresponding to the group of substituted alkanes represented as the above general formula (13) as a material in the molecule are produced as well as pre-multiplication of the bacteria is performed; and in the latter stage, the pre-cultured bacteria are made to mainly produce PHAs in the medium without a nitrogen source. Consequently, these methods enable to further increase the PHA amount accumulated in the cells.

Dicyclopropylketone, which effectively induces alkane oxidation pathway, can be added to at least one of step (1-1) and step (1-2); step (1-3) and step (1-4); and step (1-5) and step (1-6), respectively, which would make conversion of the substituted alkanes to the corresponding alkanoate having substituents effectively so that the yield of the PHA and composition ratio of the intended monomer units would become high.

Further, dicyclopropylketone alone can be used in place of the group of substituted alkanes in step 1-1, step 1-3 and step 1-5, which takes on a role of the culturing method of the first stage aiming chiefly at introducing the alkane oxidation pathway.

The temperature used in such culturing steps may be the one that enables the above strain to grow well, for



example, the range of 15-40°C, preferably the range of 20-35°C, more preferably the range of 20-30°C are appropriately selected.

For culturing, any culturing method such as liquid  
5 culture and solid culture may be used if they can multiply the microorganisms and produce the PHA comprising at least one selected from the group of 3-hydroxy-substituted alkanoate units represented as the above general formula (14) in the molecule from at  
10 least one selected from the group of substituted alkanes represented as the above general formula (13) as a material contained in the medium. Further, if the material, carbon source and oxygen are appropriately supplied, any type including batch culture, fed batch  
15 culture, semi-continuous culture, continuous culture or the like may be used. For example, a form of the liquid batch culture includes oxygen supplying methods by shaking using a shaking flask and by a stirring aeration method using a jar fermenter.

20 For the inorganic medium used in the above culturing method, any medium may be used if it contains components such as a phosphorous source (e.g. phosphate etc.), a nitrogen source (e.g. ammonium salt, nitrate, etc.) and the like capable of growing microorganisms,  
25 for example, including the MSB medium, M9 medium and the like.

In order to perform better multiplication and

accompanying PHA production, it is necessary to supplement essential trace elements by addition of, for example, about 0.3% (v/v) solution of the above trace elements into the above described inorganic salt  
5 medium.

Further for the above culturing methods, any method used for usual culture of microorganisms may be used including batch type culture, fluid batch type culture, semi-continuous culture, continuous culture,  
10 reactor type culture and solid culture.

(Extraction/purification step of PHA)

For production/acquisition of PHA from accumulating microorganism cells relating to the present invention, the above described methods  
15 performed usually may be applied.

Examples will be shown as follows. Herein, "%" as described below is the weight basis unless otherwise specified.

Examples

20 (Example 1)

The *Pseudomonas cichorii* YN2 strain was inoculated in 200 mL of the M9 medium containing 0.5% D-glucose and 0.1% FBzVA, then this was cultured with shaking at 125 strokes/min at 30°C. After 48 hours, the bacteria  
25 were recovered by centrifugal separation, resuspended with 200 mL of the M9 medium containing 0.5% D-glucose and 0.1% 5-(4-fluorobenzoyl)valeric acid (hereinafter,

sometimes abbreviated as FBzVA) but not containing a nitrogen source ( $\text{NH}_4\text{Cl}$ ), further cultured with shaking at 125 strokes/min at  $30^\circ\text{C}$ . After 40 hours, the bacteria were recovered by centrifugal separation, washed once with cold  
5 methanol and lyophilized.

This lyophilized pellet was suspended in 20 mL of chloroform and stirred at  $60^\circ\text{C}$  for 20 hours to extract PHA. After the extract was filtered through a membrane filter with the pore size of  $0.45\ \mu\text{m}$ , the filtrate was concentrated using  
10 a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the precipitate was recovered and dried in vacuo to obtain the PHA.

After methanolysis of the PHA obtained was performed according to the conventional method, the analysis by a gas  
15 chromatography-mass spectrometer (GC-MS, Shimadzu QP-5050, EI method) was carried out to identify the methyl-esterified form of the PHA monomer unit. Consequently, as shown in Table 3, the present PHA was identified to be the PHA comprising 3HFBzV as a monomer unit.

[Table 3]

Production of Polyhydroxyalkanoate by YN2 Strain

Dry cell weight (mg/L)	610
Polymer weight (mg/L)	150
Composition of monomer unit (TIC peak area ratio)	
3-Hydroxyhexanoic acid	0.2%
3-Hydroxyoctanoic acid	4.5%
3-Hydroxydecanoic acid	9.8%
3-Hydroxydodecanoic acid	4.0%
3-Hydroxydodecenoic acid	7.1%
3-Hydroxy-5-(4-fluorobenzoyl)valeric acid	74.4%

The molecular weight of the PHA was evaluated by gel permeation chromatography (GPC; Tosoh HLC-8220, Column; Polymer Laboratory PL gel MIXED-C (5  $\mu$ m), Solvent; chloroform, conversion to polystyrene). Consequently, this was  $M_n=30,000$  and  $M_w=78,000$ .

(Example 2)

The *Pseudomonas cichorii* YN2 strain was inoculated in 200 mL of the M9 medium containing 0.5% D-glucose and 0.1% FBzVA, then this was cultured with shaking at 125 strokes/min at 30°C. After 48 hours, the bacteria were recovered by centrifugal separation, washed once with cold methanol and dried in vacuo.

This vacuum dried pellet was suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract PHA. After the extract was filtered through a membrane filter with the pore size of 0.45  $\mu$ m, the filtrate was

concentrated using a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the precipitate was recovered and dried in vacuo to obtain the PHA.

5           After methanolysis of the PHA obtained was performed according to the conventional method, the analysis by a gas chromatography-mass spectrometer (GC-MS, Shimadzu QP-5050, EI method) was carried out to identify the methyl-esterified form of the PHA monomer  
10           unit. Consequently, as shown in Table 4, the present PHA was identified to be the PHA comprising 3HFBzV as a monomer unit.

[Table 4]

Production of Polyhydroxyalkanoate by YN2 Strain

Dry cell weight (mg/L)	490
Polymer weight (mg/L)	36
Composition of monomer unit (TIC peak area ratio)	
3-Hydroxybutyric acid	0.1%
3-Hydroxyhexanoic acid	0.3%
3-Hydroxyoctanoic acid	7.5%
3-Hydroxydecanoic acid	12.2%
3-Hydroxydodecanoic acid	4.6%
3-Hydroxydodecenoic acid	5.0%
3-Hydroxy-5-(4-fluorobenzoyl)valeric acid	70.3%

(Example 3)

The *Pseudomonas cichorii* YN2 strain was inoculated in 200 mL of the M9 medium containing 0.5% disodium

malate and 0.1% FBzVA, then this was cultured with shaking at 125 strokes/min at 30°C. After 4 days, the bacteria were recovered by centrifugal separation, washed once with cold methanol and dried in vacuo.

5           This vacuum dried pellet was suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract PHA. After the extract was filtered through a membrane filter with the pore size of 0.45 µm, the filtrate was concentrated using a rotary evaporator, the concentrate  
10 was reprecipitated in cold methanol, further only the precipitate was recovered and dried in vacuo to obtain the PHA.

          After methanolysis of the PHA obtained was performed according to the conventional method, the  
15 analysis by a gas chromatography-mass spectrometer (GC-MS, Shimadzu QP-5050, EI method) was carried out to identify the methyl-esterified form of the PHA monomer unit. Consequently, as shown in Table 5, the present PHA was identified to be the PHA comprising 3HFBzV as a  
20 monomer unit.

[Table 5]

Production of Polyhydroxyalkanoate by YN2 Strain

Dry cell weight (mg/L)	480
Polymer weight (mg/L)	190
Composition of monomer unit (TIC peak area ratio)	
3-Hydroxybutyric acid	60.7%
3-Hydroxyhexanoic acid	0.8%
3-Hydroxyoctanoic acid	8.3%
3-Hydroxydecanoic acid	5.1%
3-Hydroxydodecanoic acid	1.9%
3-Hydroxydodecenoic acid	1.5%
3-Hydroxy-5-(4-fluorobenzoyl)valeric acid	21.7%

(Example 4)

The *Pseudomonas cichorii* YN2 strain was inoculated in 200 mL of the M9 medium containing 0.5% yeast extract (Oriental Yeast Industry Co., Ltd.-made) and 0.1% FBzVA, then this was cultured with shaking at 125 strokes/min at 30°C. After 48 hours, the bacteria were recovered by centrifugal separation, washed once with cold methanol and dried in vacuo.

This vacuum dried pellet was suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract PHA. After the extract was filtered through a membrane filter with the pore size of 0.45 µm, the filtrate was concentrated using a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the precipitate was recovered and dried in vacuo to obtain

the PHA.

After methanolysis of the PHA obtained was performed according to the conventional method, the analysis by a gas chromatography-mass spectrometer (GC-  
5 MS, Shimadzu QP-5050, EI method) was carried out to identify the methyl-esterified form of the PHA monomer unit. Consequently, as shown in Table 6, the present PHA was identified to be the PHA comprising 3HFBzV as a monomer unit.

[Table 6]

Production of Polyhydroxyalkanoate by YN2 Strain

Dry cell weight (mg/L)	520
Polymer weight (mg/L)	60
<u>Composition of monomer unit (TIC peak area ratio)</u>	
3-Hydroxyhexanoic acid	0.8%
3-Hydroxyoctanoic acid	3.6%
3-Hydroxydecanoic acid	4.0%
3-Hydroxydodecanoic acid	1.4%
3-Hydroxy-5-(4-fluorobenzoyl)valeric acid	90.2%

(Example 5)

The *Pseudomonas cichorii* YN2 strain was inoculated in 200 mL of the M9 medium containing 0.5% polypeptone (Nippon Pharmaceutical Co., Ltd.-made) and 0.1% FBzVA, then this was cultured with shaking at 125 strokes/min at 30°C. After 48 hours, the bacteria were recovered by centrifugal separation, washed once with cold methanol and dried in vacuo.



This vacuum dried pellet was suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract PHA. After the extract was filtered through a membrane filter with the pore size of 0.45 µm, the filtrate was concentrated using a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the precipitate was recovered and dried in vacuo to obtain the PHA.

After methanolysis of the PHA obtained was performed according to the conventional method, the analysis by a gas chromatography-mass spectrometer (GC-MS, Shimadzu QP-5050, EI method) was carried out to identify the methyl-esterified form of the PHA monomer unit. Consequently, as shown in Table 7, the present PHA was identified to be the PHA comprising 3HFBzV as a monomer unit.

[Table 7]

Production of Polyhydroxyalkanoate by YN2 Strain

Dry cell weight (mg/L)	690
Polymer weight (mg/L)	290
Composition of monomer unit (TIC peak area ratio)	
3-Hydroxybutyric acid	1.2%
3-Hydroxyhexanoic acid	0.3%
3-Hydroxyoctanoic acid	4.7%
3-Hydroxydecanoic acid	9.8%
3-Hydroxydodecanoic acid	3.1%
3-Hydroxydodecenoic acid	3.5%
3-Hydroxy-5-(4-fluorobenzoyl)valeric acid	77.4%

(Example 6)

The *Pseudomonas cichorii* H45 strain was inoculated in 200 mL of the M9 medium containing 0.5% D-glucose and 0.1% FBzVA, then this was cultured with shaking at 125 strokes/min at 30°C. After 48 hours, the bacteria were recovered by centrifugal separation, resuspended with 200 mL of the M9 medium containing 0.5% D-glucose and 0.1% FBzVA but not containing a nitrogen source (NH<sub>4</sub>Cl), further cultured with shaking at 125 strokes/min at 30°C. After 40 hours, the bacteria were recovered by centrifugal separation, washed once with cold methanol and lyophilized.

This lyophilized pellet was suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract PHA. After the extract was filtered through a membrane filter with the pore size of 0.45 µm, the filtrate was concentrated using a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the precipitate was recovered and dried in vacuo to obtain the PHA.

After methanolysis of the PHA was performed according to the conventional method, the analysis by a gas chromatography-mass spectrometer (GC-MS, Shimadzu QP-5050, EI method) was carried out to identify the methyl-esterified form of the PHA monomer unit.

Consequently, as shown in Table 8, the present PHA was identified to be the PHA comprising 3HFBzV as a monomer

unit.

[Table 8]

Production of Polyhydroxyalkanoate by H45 Strain

Dry cell weight (mg/L)	490
Polymer weight (mg/L)	90
<u>Composition of monomer unit (TIC peak area ratio)</u>	
3-Hydroxyhexanoic acid	0.1%
3-Hydroxyoctanoic acid	4.0%
3-Hydroxydecanoic acid	8.8%
3-Hydroxydodecanoic acid	5.1%
3-Hydroxydodecenoic acid	7.8%
3-Hydroxy-5-(4-fluorobenzoyl)valeric acid	74.2%

The molecular weight of this PHA was evaluated by gel permeation chromatography (GPC; Tosoh HLC-8220, Column; Polymer Laboratory PL gel MIXED-C (5  $\mu$ m), Solvent; chloroform, conversion to polystyrene). Consequently, this was  $M_n=26,000$  and  $M_w=61,000$ .

(Example 7)

The *Pseudomonas jessenii* P161 strain was inoculated in 200 mL of the M9 medium containing 0.5% D-glucose and 0.1% FBzVA, then this was cultured with shaking at 125 strokes/min at 30°C. After 48 hours, the bacteria were recovered by centrifugal separation, resuspended with 200 mL of the M9 medium containing 0.5% D-glucose and 0.1% FBzVA but not containing a nitrogen source ( $NH_4Cl$ ), further cultured with shaking at 125 strokes/min at 30°C. After 40 hours, the

bacteria were recovered by centrifugal separation,  
washed once with cold methanol and lyophilized.

This lyophilized pellet was suspended in 20 mL of  
chloroform and stirred at 60°C for 20 hours to extract  
5 PHA. After the extract was filtered through a membrane  
filter with the pore size of 0.45 µm, the filtrate was  
concentrated using a rotary evaporator, the concentrate  
was reprecipitated in cold methanol, further only the  
precipitate was recovered and dried in vacuo to obtain  
10 the PHA.

After methanolysis of the PHA was performed  
according to the conventional method, the analysis by a  
gas chromatography-mass spectrometer (GC-MS, Shimadzu  
QP-5050, EI method) was carried out to identify the  
15 methyl-esterified form of the PHA monomer unit.  
Consequently, as shown in Table 9, the present PHA was  
identified to be the PHA comprising 3HFBzV as a monomer  
unit.

[Table 9]

Production of Polyhydroxyalkanoate by P161 Strain

Dry cell weight (mg/L)	590
Polymer weight (mg/L)	110
Composition of monomer unit (TIC peak area ratio)	
3-Hydroxyoctanoic acid	3.5%
3-Hydroxydecanoic acid	8.0%
3-Hydroxydodecanoic acid	4.9%
3-Hydroxydodecenoic acid	5.6%
3-Hydroxy-5-(4-fluorobenzoyl)valeric acid	78.0%

The molecular weight of this PHA was evaluated by gel permeation chromatography (GPC; Tosoh HLC-8220, Column; Polymer Laboratory PL gel MIXED-C (5  $\mu$ m), Solvent; chloroform, conversion to polystyrene).

5 Consequently, this was  $M_n=41,000$  and  $M_w=110,000$ .

(Example 8)

200 mL of the M9 medium containing 0.5% (w/v) polypeptone and n-amylbenzene (3 concentrations: 0.025%, 0.05% and 0.1% (v/v)) was prepared, placed into  
10 a 500 mL volume shaking flask and sterilized by an autoclave. Each flask was returned to a room temperature and the YN2 strain on the agar plate was inoculated, then this was cultured with shaking at 125 strokes/min at 30°C for 24 hours. After completion of  
15 the culture, the bacteria were recovered by centrifugal separation, washed once with cold methanol and lyophilized.

This lyophilized pellet was weighed, then suspended in 20 mL of chloroform and stirred at 60°C  
20 for 20 hours to extract PHA. After the extract was filtered through a membrane filter with the pore size of 0.45  $\mu$ m, the filtrate was concentrated using a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the precipitate was  
25 recovered and dried in vacuo to obtain the PHA and weigh it. Each yield is shown in Table 10.

The molecular weight of this PHA obtained in the

0.05% amylbenzene system was evaluated by gel permeation chromatography (GPC; Tosoh HLC-8220, Column; Polymer Laboratory PL gel MIXED-C (5  $\mu$ m), Solvent; chloroform, conversion to polystyrene). Consequently, the number average molecular weight ( $M_n$ ) was  $M_n=90,000$  and the molecular weight distribution is 1.9.

Composition of the PHA obtained was analyzed as follows. That is, about 10 mg of the PHA was placed into a 25 mL volume pear-shape flask, dissolved in 2 mL chloroform, and to this solution, 2 mL of a methanol solution containing 3% sulfuric acid was added, and the mixture was reacted for 3.5 hours refluxing at 100°C.

After completion of the reaction, 10 mL of deionized water was added, shaken vigorously for 10 min, then the lower chloroform layer separated into two layers was taken out, dehydrated with magnesium sulfate, then this chloroform layer was submitted to a gas chromatography-mass spectrometer (GC-MS, Shimadzu QP-5050, EI method) to identify the methyl-esterified form of the PHA monomer unit. The results are shown in Table 11.

Further, the mass spectra of peaks obtained by GC-MS analysis of 0.1% amylbenzene system are shown in Figs. 1 to 4 (corresponding to methyl esters of Fig. 1: 3-hydroxybutyric acid, Fig. 2: 3-hydroxyoctanoic acid, Fig. 3: 3-hydroxydecanoic acid, Fig. 4: and 3-hydroxy-5-phenylvaleric acid, respectively).

[Table 10]

AMB (%)	CDW (mg/L)	PDW (mg/L)	Yield (%)
0.025	900	65	7.2
0.05	1050	200	19.0
0.1	850	65	7.6

AMB: amylbenzene, CDW: dry cell weight,

PDW: dry polymer cell weight,

Yield:  $PDW/CDW \times 100$

[Table 11]

AMB (%)	3HB	3HO	3HD	3HPV
0.025	51.1	0.7	2.1	46.1
0.05	19.2	0.7	3.6	76.5
0.1	24.6	2.1	3.8	72.5

AMB: amylbenzene, 3HB: 3-hydroxybutyric acid,

3HO: 3-hydroxyoctanoic acid,

3HD: 3-hydroxydecanoic acid,

3HPV: 3-hydroxy-5-phenylvaleric acid

(Example 9)

200 mL of the M9 medium containing 0.5% (w/v) sodium glutamate and n-amylbenzene (0.05% and 0.1% (v/v)) was prepared, placed into a 500 mL volume shaking flask and sterilized by an autoclave.

The flask was returned to a room temperature and the YN2 strain on the agar plate was inoculated, then this was cultured with shaking at 125 strokes/min at

30°C for 26 hours.

After completion of the culture, the bacteria were recovered by centrifugal separation, transferred to the M9 medium without the  $\text{NH}_4\text{Cl}$  component (concentrations of sodium glutamate and amylbenzene are same), and cultured with shaking at 125 strokes/min at 30°C for 20 hours.

After completion of the culture, the bacteria was recovered by centrifugal separation, washed once with cold methanol and lyophilized.

This lyophilized pellet was weighed, then suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract PHA. After the extract was filtered through a membrane filter with the pore size of 0.45  $\mu\text{m}$ , the filtrate was concentrated using a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the precipitate was recovered and dried in vacuo to obtain the PHA and weigh it. Each yield is shown in Table 12.

Composition of the PHA obtained was analyzed by the method similar to Example 8. The results are shown in Table 13.

[Table 12]

CDW (mg/L)	PDW (mg/L)	Yield (%)
900	320	35.6

CDW: dry cell weight,



PDW: dry polymer cell weight,

Yield:  $PDW/CDW \times 100$

[Table 13]

3HB	3HD	3HPV
88.7	3.1	8.2

3HB: 3-hydroxybutyric acid,

3HD: 3-hydroxydecanoic acid,

3HPV: 3-hydroxy-5-phenylvaleric acid

(Example 10)

200 mL of the M9 medium containing 0.5% (w/v) polypeptone and n-hexanophenone (4 concentrations: 0.01%, 0.025%, 0.05% and 0.1% (v/v)) was prepared, placed into a 500 mL volume shaking flask and sterilized by an autoclave.

Each flask was returned to a room temperature and the *Pseudomonas cichorii* YN2 strain was inoculated, then this was cultured with shaking at 125 strokes/min at 30°C. After 48 hours, the bacteria were recovered by centrifugal separation, washed once with cold methanol and lyophilized.

This lyophilized pellet was suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract PHA. After the extract was filtered through a membrane filter with the pore size of 0.45  $\mu$ m, the filtrate was concentrated using a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the

precipitate was recovered and dried in vacuo to obtain the PHA. Each yield is shown in Tables 14 to 17 (Table 14: Results of 0.01% n-hexanophenone, Table 15: Results of 0.025% n-hexanophenone, Table 16: Results of 0.05% n-hexanophenone, Table 17: Results of 0.1% n-hexanophenone).

[Table 14]

Dry cell weight	815 mg/L
Dry polymer weight	50 mg/L
Dry polymer weight/Dry cell weight	6.1%
Composition of monomer unit (TIC peak area ratio)	
3-Hydroxybutyric acid	42.4%
3-Hydroxyhexanoic acid	0.0%
3-Hydroxyoctanoic acid	5.2%
3-Hydroxydecanoic acid	13.8%
3-Hydroxydodecanoic acid	12.1%
3-Hydroxydodecenoic acid	3.7%
3-Hydroxy-5-benzoylvaleric acid	22.8%

[Table 15]

Dry cell weight	775 mg/L
Dry polymer weight	60 mg/L
Dry polymer weight/Dry cell weight	7.7%
Composition of monomer unit (TIC peak area ratio)	
3-Hydroxybutyric acid	32.8%
3-Hydroxyhexanoic acid	0.0%
3-Hydroxyoctanoic acid	3.3%
3-Hydroxydecanoic acid	12.4%
3-Hydroxydodecanoic acid	12.9%
3-Hydroxydodecenoic acid	3.8%
3-Hydroxy-5-benzoylvaleric acid	34.8%

[Table 16]

Dry cell weight	685 mg/L
Dry polymer weight	80 mg/L
Dry polymer weight/Dry cell weight	11.7%
Composition of monomer unit (TIC peak area ratio)	
3-Hydroxybutyric acid	21.7%
3-Hydroxyhexanoic acid	0.0%
3-Hydroxyoctanoic acid	4.2%
3-Hydroxydecanoic acid	12.1%
3-Hydroxydodecanoic acid	12.0%
3-Hydroxydodecenoic acid	2.8%
3-Hydroxy-5-benzoylvaleric acid	47.2%

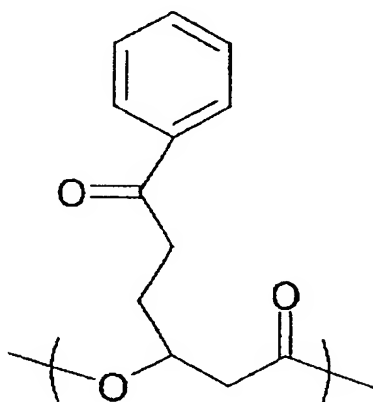
[Table 17]

Dry cell weight	755 mg/L
Dry polymer weight	70 mg/L
Dry polymer weight/Dry cell weight	9.3%
Composition of monomer unit (TIC peak area ratio)	
3-Hydroxybutyric acid	12.6%
3-Hydroxyhexanoic acid	0.2%
3-Hydroxyoctanoic acid	2.3%
3-Hydroxydecanoic acid	7.7%
3-Hydroxydodecanoic acid	8.0%
3-Hydroxydodecenoic acid	1.7%
3-Hydroxy-5-benzoylvaleric acid	60.5%

The molecular weight of the PHA obtained (use of 0.1% (v/v) n-hexanophenone) was evaluated by gel permeation chromatography (GPC; Tosoh HLC-8220, Column; Tosoh TSK-GEL Super HM-H, Solvent; chloroform, conversion to polystyrene). Consequently, this was Mn=68,000 and Mw=454,000.

Further, after methanolysis of the PHA was performed according to the conventional method, the analysis by a gas chromatography-mass spectrometer (GC-MS, Shimadzu QP-5050, EI method) was carried out to identify the methyl-esterified form of the PHA monomer unit. The results are shown in Tables 14 to 17. Consequently, as shown in Tables 14 to 17, the present PHA was identified to be the PHA comprising 3-hydroxy-5-benzoylvaleric acid (hereinafter, abbreviated as 3HBV

if necessary) represented by the chemical formula (31) as a monomer unit.



(31)

The compound was analyzed using the NMR apparatus in the following conditions.

<Measuring apparatus> FT-NMR: Bruker DPX 400

Resonance frequency: <sup>1</sup>H=400 MHz

<Measuring apparatus> Measuring nuclide: <sup>1</sup>H

Solvent used: CDCl<sub>3</sub>

Reference: capillary-sealed CDCl<sub>3</sub>

Measuring temperature: room temperature

The <sup>1</sup>H-NMR spectrum chart is shown in Fig. 5 and the assignment results are shown in Table 18, respectively.

[Table 18]

Chemical shift (ppm)	Integrated value	type	Position
2.04	2	m	d
2.56	2	m	b
3.00	2	m	e
5.26	1	m	c
7.36	2	m	i, k
7.46	1	t	j
7.89	2	d	h, l

(Example 11)

200 mL of the M9 medium containing 0.5% (w/v) sodium glutamate and 0.1% (v/v) n-hexanophenone was prepared, placed into a 500 mL volume shaking flask and sterilized by an autoclave.

The flask was returned to a room temperature and the *Pseudomonas cichorii* YN2 strain on the agar plate was inoculated, then this was cultured with shaking at 125 strokes/min at 30°C. After 48 hours, the bacteria were recovered by centrifugal separation, washed once with cold methanol and lyophilized.

This lyophilized pellet was suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract PHA. After the extract was filtered through a membrane filter with the pore size of 0.45 µm, the filtrate was concentrated using a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the

precipitate was recovered and dried in vacuo to obtain the PHA.

After methanolysis of the PHA obtained was performed according to the conventional method, the analysis by a gas chromatography-mass spectrometer (GC-MS, Shimadzu QP-5050, EI method) was carried out to identify the methyl-esterified form of the PHA monomer unit. The results are shown in Table 19.

Consequently, as shown in Table 19, the present PHA was identified to be the PHA comprising 3HBV represented by the chemical formula (31) as a monomer unit.

[Table 19]

Dry cell weight	1040 mg/L
Dry polymer weight	445 mg/L
Dry polymer weight/Dry cell weight	42.8%
Composition of monomer unit (TIC peak area ratio)	
3-Hydroxybutyric acid	39.4%
3-Hydroxyhexanoic acid	0.3%
3-Hydroxyoctanoic acid	3.9%
3-Hydroxydecanoic acid	11.01%
3-Hydroxydodecanoic acid	6.5%
3-Hydroxydodecenoic acid	8.3%
3-Hydroxy-5-benzoylvaleric acid	30.5%

(Example 12)

200 mL of the M9 medium containing 0.5% (w/v) yeast extract and 0.1% (v/v) n-hexanophenone was prepared, placed into a 500 mL volume shaking flask and

sterilized by an autoclave.

The flask was returned to a room temperature and the *Pseudomonas cichorii* YN2 strain on the agar plate was inoculated, then this was cultured with shaking at  
5 125 strokes/min at 30°C. After 48 hours, the bacteria were recovered by centrifugal separation, washed once with cold methanol and lyophilized.

This lyophilized pellet was suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract  
10 PHA. After the extract was filtered through a membrane filter with the pore size of 0.45 µm, the filtrate was concentrated using a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the precipitate was recovered and dried in vacuo to obtain  
15 the PHA.

After methanolysis of the PHA obtained was performed according to the conventional method, the analysis by a gas chromatography-mass spectrometer (GC-MS, Shimadzu QP-5050, EI method) was carried out to  
20 identify the methyl-esterified form of the PHA monomer unit. The results are shown in Table 20. Consequently, as shown in Table 20, the present PHA was identified to be the PHA comprising 3HBV represented by the chemical formula (31) as a monomer unit.



[Table 20]

Dry cell weight	925 mg/L
Dry polymer weight	25 mg/L
Dry polymer weight/Dry cell weight	2.7%
Composition of monomer unit (TIC peak area ratio)	
3-Hydroxybutyric acid	73.5%
3-Hydroxyhexanoic acid	0.0%
3-Hydroxyoctanoic acid	2.0%
3-Hydroxydecanoic acid	3.7%
3-Hydroxydodecanoic acid	0.0%
3-Hydroxydodecenoic acid	2.0%
3-Hydroxy-5-benzoylvaleric acid	18.8%

(Example 13)

200 mL of the M9 medium containing 0.5% (w/v) sodium glutamate and 0.1% (v/v) n-phenoxy pentane was prepared, placed into a 500 mL volume shaking flask and sterilized by an autoclave.

The flask was returned to a room temperature and the *Pseudomonas cichorii* YN2 strain on the agar plate was inoculated, then this was cultured with shaking at 125 strokes/min at 30°C. After 120 hours, the bacteria were recovered by centrifugal separation, washed once with cold methanol and lyophilized.

This lyophilized pellet was suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract PHA. After the extract was filtered through a membrane filter with the pore size of 0.45 µm, the filtrate was

concentrated using a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the precipitate was recovered and dried in vacuo to obtain 23 mg of the PHA.

5           The molecular weight of this PHA was evaluated by gel permeation chromatography (GPC; Tosoh HLC-8220, Column; Tosoh TSK-GEL Super HM-H, Solvent; chloroform, conversion to polystyrene). Consequently, this was  $M_n=64,000$  and  $M_w=141,000$ .

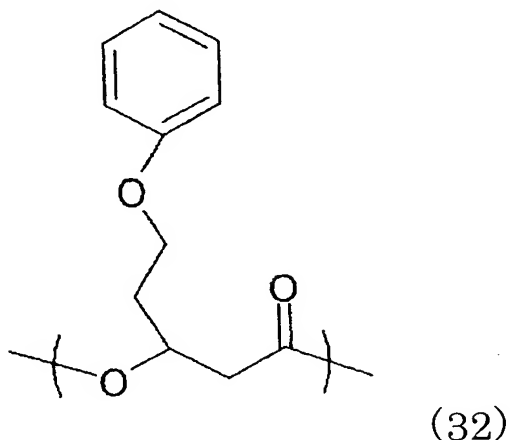
10           Further, after methanolysis of the PHA obtained was performed according to the conventional method, the analysis by a gas chromatography-mass spectrometer (GC-MS, Shimadzu QP-5050, EI method) was carried out to identify the methyl-esterified form of the PHA monomer  
15           unit. The results are shown in Table 21.

[Table 21]

Production of PHA Produced in Example 13 and  
Composition of Monomer Unit

Dry cell weight	570 mg/L
Dry polymer weight	115 mg/L
Dry polymer weight/Dry cell weight	20.2%
Composition of monomer unit (TIC peak area ratio)	
3-Hydroxybutyric acid	15.0%
3-Hydroxyvaleric acid	0.3%
3-Hydroxyhexanoic acid	0.1%
3-Hydroxyoctanoic acid	1.0%
3-Hydroxydecanoic acid	1.0%
3-Hydroxydodecanoic acid	0.3%
3-Hydroxydodecenoic acid	0.8%
3-Hydroxy-5-phenoxyvaleric acid	81.5%

Consequently, as shown in Table 21, the present PHA was identified to be the PHA comprising 3-hydroxy-5-phenoxyvaleric acid (hereinafter, abbreviated as 3HPxV) represented by the chemical formula (32) as a monomer unit.



(Example 14)

200 mL of the M9 medium containing 0.5% (w/v) polypeptone and 0.1% (v/v) n-phenoxy-pentane was prepared, placed into a 500 mL volume shaking flask and sterilized by an autoclave.

The flask was returned to a room temperature and the *Pseudomonas cichorii* YN2 strain on the agar plate was inoculated, then this was cultured with shaking at 125 strokes/min at 30°C. After 120 hours, the bacteria were recovered by centrifugal separation, washed once with cold methanol and lyophilized.

This lyophilized pellet was suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract PHA. After the extract was filtered through a membrane

filter with the pore size of 0.45  $\mu\text{m}$ , the filtrate was concentrated using a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the precipitate was recovered and dried in vacuo to obtain  
5 2 mg of the PHA.

After methanolysis of the PHA obtained was performed according to the conventional method, the analysis by a gas chromatography-mass spectrometer (GC-MS, Shimadzu QP-5050, EI method) was carried out to  
10 identify the methyl-esterified form of the PHA monomer unit. The results are shown in Table 22.

Consequently, as shown in Table 22, the present PHA was identified to be the PHA comprising 3HPxV represented by the chemical formula (32) as a monomer unit.

[Table 22]

Production of PHA Produced in Example 14 and  
Composition of Monomer Unit

Dry cell weight	560 mg/L
Dry polymer weight	10 mg/L
Dry polymer weight/Dry cell weight	1.8%
Composition of monomer unit (TIC peak area ratio)	
3-Hydroxybutyric acid	1.8%
3-Hydroxyhexanoic acid	0.0%
3-Hydroxyoctanoic acid	0.0%
3-Hydroxydecanoic acid	0.0%
3-Hydroxydodecanoic acid	0.0%
3-Hydroxydodecenoic acid	0.0%
3-Hydroxy-5-phenoxyvaleric acid	98.2%

(Example 15)

(Synthesis of 1-(4-fluorophenyl)-1-hexanone

(FPHxO))

100 mL of tetrahydrofuran was placed into a four-neck round-bottom flask, then 7.92 g (0.05 mol) of 4-fluorobenzoyl chloride and 0.53 g (1.5 mmol) of tris(acetylacetonate)iron (III) were added and stirred under a nitrogen atmosphere. To this solution pentylmagnesium bromide was added at a room temperature and stirred at a room temperature for 10 min. After completion of the reaction, this solution was acidified with dilute hydrochloric acid and the organic phase was extracted with diethyl ether. Further, the organic phase was neutralized with satd. sodium

hydrogencarbonate solution and washed with satd. sodium chloride solution. The organic phase was dehydrated with anhydrous magnesium sulfate, then diethyl ether was evaporated by a rotary evaporator and dried by a vacuum pump to obtain crude FPHxO.

The purification was performed by being isolated by silica gel column chromatography (developing solvent: n-hexane : ethyl acetate=30 : 1) followed by being recrystallized with n-hexane to obtain 5.23 g of FPHxO.

The compound obtained was analyzed with NMR in the following conditions.

<Measuring apparatus> FT-NMR: Bruker DPX 400

Resonance frequency:  $^1\text{H}$ =400 MHz

<Measuring apparatus> Measuring nuclide:  $^1\text{H}$

Solvent used:  $\text{CDCl}_3$

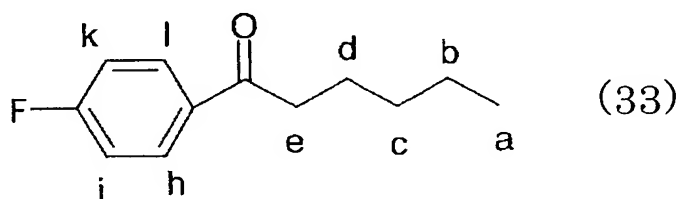
Reference: capillary-sealed TMS/ $\text{CDCl}_3$

Measuring temperature: room temperature

The  $^1\text{H}$ -NMR spectrum is shown in Fig. 7 and the assignment results (see chemical formula (33)) are shown in Table 23, respectively.

[Table 23]

Chemical shift (ppm)	Integrated value	type	Position
0.91	3	m	a
1.36	4	m	b, c
1.73	2	m	d
2.92	2	quart	e
7.13	2	m	i, k
7.99	2	m	h, l



The purified substance was analyzed using a gas chromatography-mass spectrometer (GC-MS, Shimadzu QP-5050, EI method) to be identified. The data of the GC-MS spectrum are shown in Fig. 8. As a result, the GC-MS TIC area ratio of FPHxO was 87%.

(Example 16)

The *Pseudomonas cichorii* YN2 strain was inoculated in 200 mL of the M9 medium containing 0.5% D-glucose and 0.05% FPHxO, then this was cultured with shaking at 125 strokes/min at 30°C. After 5 days, the bacteria were recovered by centrifugal separation, suspended with 10% sodium hypochlorite solution, shaken at 4°C for 2 hours and the PHA was extracted. The precipitate

from the extract was recovered by centrifugal separation, washed with water and then dried in vacuo to obtain the PHA.

5 The PHA obtained was analyzed using the NMR apparatus (FT-NMR: Bruker DPX 400) in the following measuring conditions.

<Measuring condition> Measuring nuclide:  $^1\text{H}$

Solvent used:  $\text{CDCl}_3$  (capillary-sealed TMS/ $\text{CDCl}_3$  used as reference)

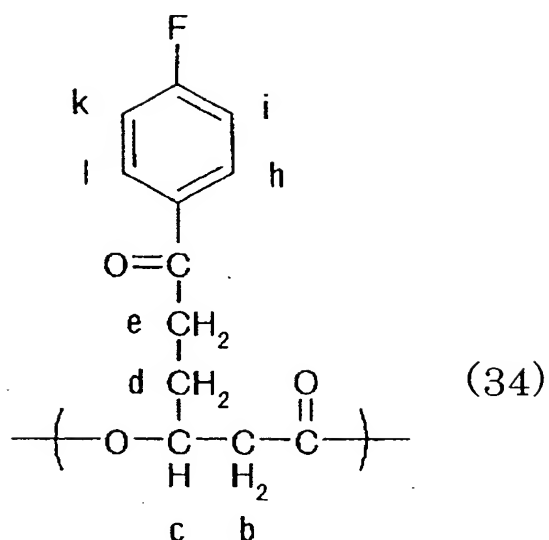
10 Resonance frequency:  $^1\text{H}=400\text{MHz}$

The  $^1\text{H}$ -NMR spectrum is shown in Fig. 9 and the assignment results (see chemical formula (34)) are shown in Table 24, respectively.

[Table 24]

Chemical shift (ppm)	Integrated value	type	Position
2.01 - 2.13	2	m	d
2.44 - 2.70	2	m	b
2.91 - 3.07	2	m	e
5.20 - 5.32	1	m	c
6.99 - 7.13	2	m	i, k
7.87 - 8.01	2	m	h, l





After methanolysis of the PHA obtained was performed according to the conventional method, the analysis by a gas chromatography-mass spectrometer (GC-MS, Shimadzu QP-5050, EI method) was carried out to identify the methyl-esterified form of the PHA monomer unit. Consequently, as shown in Table 25, the present PHA was identified to be the PHA comprising 3-hydroxy-5-(4-fluorobenzoyl)valeric acid (hereinafter sometimes abbreviated as 3HFBzV) as a monomer unit.

[Table 25]

Production of Polyhydroxyalkanoate by YN2 Strain

Polymer weight (mg/L)	27
Composition of monomer unit (TIC peak area ratio)	
3-Hydroxybutyric acid	2.7%
3-Hydroxyhexanoic acid	0.6%
3-Hydroxyheptanoic acid	0.1%
3-Hydroxyoctanoic acid	8.1%
3-Hydroxynonanoic acid	0.1%
3-Hydroxydecanoic acid	11.0%
3-Hydroxydodecanoic acid	5.1%
3-Hydroxydodecenoic acid	0.1%
3-Hydroxytetradecanoic acid	1.9%
3-Hydroxy-5-(4-fluorobenzoyl)valeric acid	70.4%

The molecular weight of this PHA was evaluated by gel permeation chromatography (GPC; Tosoh HLC-8220, Column; Polymer Laboratory PL gel MIXED-C (5  $\mu$ m), Solvent; chloroform, conversion to polystyrene). Consequently, this was Mn=26,000 and Mw=142,000.

(Example 17)

The *Pseudomonas cichorii* YN2 strain was inoculated in 200 mL of the M9 medium containing 0.5% D-glucose and 0.1% FPHxO, then this was cultured with shaking at 125 strokes/min at 30°C. After 48 hours, the bacteria were recovered by centrifugal separation, washed once with cold methanol and dried in vacuo.

This vacuum dried pellet was suspended in 20 mL of

chloroform and stirred at 60°C for 20 hours to extract PHA. After the extract was filtered through a membrane filter with the pore size of 0.45 µm, the filtrate was concentrated using a rotary evaporator, the concentrate  
5 was reprecipitated in cold methanol, further only the precipitate was recovered and dried in vacuo to obtain the PHA.

After methanolysis of the PHA obtained was performed according to the conventional method, the  
10 analysis by a gas chromatography-mass spectrometer (GC-MS, Shimadzu QP-5050, EI method) was carried out to identify the methyl-esterified form of the PHA monomer unit. The results are shown in Table 26.

[Table 26]

Production of Polyhydroxyalkanoate by YN2 Strain

Dry cell weight (mg/L)	500
Polymer weight (mg/L)	7.5
<u>Composition of monomer unit (TIC peak area ratio)</u>	
3-Hydroxybutyric acid	2.0%
3-Hydroxyhexanoic acid	0.4%
3-Hydroxyoctanoic acid	7.1%
3-Hydroxydecanoic acid	7.2%
3-Hydroxydodecanoic acid	2.3%
3-Hydroxydodecenoic acid	2.1%
3-Hydroxytetradecanoic acid	0.3%
3-Hydroxy-5-(4-fluorobenzoyl)valeric acid	78.6%

From the above results, the present PHA was

identified to be the PHA comprising 3HFBzV as a monomer unit.

(Example 18)

The *Pseudomonas cichorii* YN2 strain was inoculated  
5 in 200 mL of the M9 medium containing 0.5% sodium  
glutamate and 0.1% FPHxO, then this was cultured with  
shaking at 125 strokes/min at 30°C. After 7 days, the  
bacteria were recovered by centrifugal separation,  
washed once with cold methanol and dried in vacuo.

10 This vacuum dried pellet was suspended in 20 mL of  
chloroform and stirred at 60°C for 20 hours to extract  
PHA. After the extract was filtered through a membrane  
filter with the pore size of 0.45 µm, the filtrate was  
concentrated using a rotary evaporator, the concentrate  
15 was reprecipitated in cold methanol, further only the  
precipitate was recovered and dried in vacuo to obtain  
the PHA.

After methanolysis of the PHA obtained was  
performed according to the conventional method, the  
20 analysis by a gas chromatography-mass spectrometer (GC-  
MS, Shimadzu QP-5050, EI method) was carried out to  
identify the methyl-esterified form of the PHA monomer  
unit. The results are shown in Table 27.

[Table 27]

Production of Polyhydroxyalkanoate by YN2 Strain

Dry cell weight (mg/L)	490
Polymer weight (mg/L)	250
Composition of monomer unit (TIC peak area ratio)	
3-Hydroxybutyric acid	56.8%
3-Hydroxyvaleric acid	0.6%
3-Hydroxyhexanoic acid	0.5%
3-Hydroxyoctanoic acid	7.2%
3-Hydroxydecanoic acid	7.1%
3-Hydroxydodecanoic acid	2.0%
3-Hydroxydodecenoic acid	1.8%
3-Hydroxy-5-(4-fluorobenzoyl)valeric acid	24.0%

From the above results, the present PHA was identified to be the PHA comprising 3HFBzV as a monomer unit.

(Example 19)

The *Pseudomonas cichorii* YN2 strain was inoculated in 200 mL of the M9 medium containing 0.5% sodium glutamate and 0.1% FPHxO, then this was cultured with shaking at 125 strokes/min at 30°C. After 48 hours, the bacteria were recovered by centrifugal separation, washed once with cold methanol and dried in vacuo.

This vacuum dried pellet was suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract PHA. After the extract was filtered through a membrane filter with the pore size of 0.45  $\mu$ m, the filtrate was

concentrated using a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the precipitate was recovered and dried in vacuo to obtain the PHA.

5           After methanolysis of the PHA obtained was performed according to the conventional method, the analysis by a gas chromatography-mass spectrometer (GC-MS, Shimadzu QP-5050, EI method) was carried out to identify the methyl-esterified form of the PHA monomer  
10 unit. The results are shown in Table 28.

[Table 28]

Production of Polyhydroxyalkanoate by YN2 Strain

Dry cell weight (mg/L)	410
Polymer weight (mg/L)	38.
Composition of monomer unit (TIC peak area ratio)	
3-Hydroxybutyric acid	17.4%
3-Hydroxyvaleric acid	0.8%
3-Hydroxyhexanoic acid	0.9%
3-Hydroxyheptanoic acid	0.1%
3-Hydroxyoctanoic acid	12.9%
3-Hydroxynonanoic acid	0.2%
3-Hydroxydecanoic acid	14.0%
3-Hydroxydodecanoic acid	5.1%
3-Hydroxydodecenoic acid	3.8%
3-Hydroxytetradecanoic acid	0.4%
3-Hydroxy-5-(4-fluorobenzoyl)valeric acid	44.4%

From the above results, the present PHA was identified to be the PHA comprising 3HFBzV as a monomer

unit.

(Example 20)

200 mL of the M9 medium containing 0.5% (w/v) polypeptone and 0.1% (v/v) n-phenoxyheptane was  
5 prepared, placed into a 500 mL volume shaking flask and sterilized by an autoclave.

The flask was returned to a room temperature and the *Pseudomonas cichorii* YN2 strain on the agar plate was inoculated, then this was cultured with shaking at  
10 125 strokes/min at 30°C. After 120 hours, the bacteria were recovered by centrifugal separation, washed once with cold methanol and lyophilized.

This lyophilized pellet was suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract  
15 PHA. After the extract was filtered through a membrane filter with the pore size of 0.45 µm, the filtrate was concentrated using a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the precipitate was recovered and dried in vacuo to obtain  
20 4 mg of the PHA.

The molecular weight of this PHA was evaluated by gel permeation chromatography (GPC; Tosoh HLC-8220, Column; Tosoh TSK-GEL Super HM-H, Solvent; chloroform, conversion to polystyrene). Consequently, this was  
25 Mn=52,000 and Mw=122,000.

After methanolysis of the PHA obtained was performed according to the conventional method, the

analysis by a gas chromatography-mass spectrometer (GC-MS, Shimadzu QP-5050, EI method) was carried out to identify the methyl-esterified form of the PHA monomer unit. The results are shown in Table 29.

- 5           Consequently, as shown in Table 29, the present PHA was identified to be the PHA comprising 3-hydroxy-5-phenoxyvaleric acid and 3-hydroxy-7-phenoxyheptanoic acid as monomer units.

[Table 29]

Production of PHA Produced in Example 20 and  
Composition of Monomer Unit

Dry cell weight	620 mg/L
Dry polymer weight	20 mg/L
Dry polymer weight/Dry cell weight	3.2%
Composition of monomer unit (peak area ratio)	
3-Hydroxybutyric acid	1.4%
3-Hydroxyhexanoic acid	0.0%
3-Hydroxyoctanoic acid	0.1%
3-Hydroxydecanoic acid	0.2%
3-Hydroxydodecanoic acid	0.0%
3-Hydroxydodecenoic acid	0.0%
3-Hydroxy-5-phenoxyvaleric acid	29.7%
3-Hydroxy-7-phenoxyheptanoic acid	68.6%

(Example 21)

200 mL of the M9 medium containing 0.5% (w/v) glucose was prepared, placed into a 500 mL volume shaking flask and sterilized by an autoclave. The flask was returned to a room temperature and 5-(4-



vinylphenyl)pentane sterilized by a filter was added with well stirring so that the concentration is adjusted to 0.1% (v/v), then the *Pseudomonas cichorii* YN2 strain was inoculated and cultured with shaking at 125 strokes/min at 30°C. After 120 hours, the bacteria were recovered by centrifugal separation.

Then, 200 mL of the M9 medium containing 0.5% (w/v) glucose but not containing  $\text{NH}_4\text{Cl}$  as a nitrogen source was prepared, placed into a 500 mL volume shaking flask and sterilized by an autoclave. The flask was returned to a room temperature and 5-(4-vinylphenyl)pentane sterilized by a filter was added with well stirring so that the concentration is adjusted to 0.1% (v/v), then the recovered bacteria was resuspended in the medium and cultured with shaking at 125 strokes/min at 30°C. After 120 hours, the bacteria were recovered by centrifugal separation, washed once with cold methanol and lyophilized.

This lyophilized pellet was suspended in 20 mL of chloroform and stirred at 30°C for 48 hours to extract PHA. After the extract was filtered through a membrane filter with the pore size of 0.45  $\mu\text{m}$ , the filtrate was concentrated using a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the precipitate was recovered and dried in vacuo to obtain 3 mg of the PHA.

The molecular weight of this PHA obtained was

obtained by performing the GPC analysis using the method similar to Example 10. Consequently, this was  $M_n=12,000$  and  $M_w=21,000$ . When performing the  $^1H$ -NMR analysis of the PHA obtained using the method similar to Example 10, it was confirmed to be the PHA containing 97% 3-hydroxy-5-(4-vinylphenyl)valeric acid unit and 3-hydroxybutyric acid as the other unit.

(Example 22)

200 mL of the M9 medium containing 0.5% (w/v) polypeptone was prepared, placed into a 500 mL volume shaking flask and sterilized by an autoclave. The flask was returned to a room temperature and 5-(4-vinylphenyl)pentane sterilized by a filter was added with well stirring so that the concentration is adjusted to 0.1% (v/v), then the *Pseudomonas cichorii* YN2 strain was inoculated and cultured with shaking at 125 strokes/min at 30°C. After 120 hours, the bacteria were recovered by centrifugal separation.

Then, 200 mL of the M9 medium containing 0.5% (w/v) sodium pyruvate but not containing  $NH_4Cl$  as a nitrogen source was prepared, placed into a 500 mL volume shaking flask and sterilized by an autoclave. The flask was returned to a room temperature and 5-(4-vinylphenyl)pentane sterilized by a filter was added with well stirring so that the concentration is adjusted to 0.1% (v/v), then the recovered bacteria was resuspended in the medium and cultured with shaking at

125 strokes/min at 30°C. After 120 hours, the bacteria were recovered by centrifugal separation, washed once with cold methanol and lyophilized.

5 This lyophilized pellet was suspended in 20 mL of chloroform and stirred at 30°C for 48 hours to extract PHA. After the extract was filtered through a membrane filter with the pore size of 0.45 µm, the filtrate was concentrated using a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the  
10 precipitate was recovered and dried in vacuo to obtain 5 mg of the PHA.

The molecular weight of this PHA obtained was obtained by performing the GPC analysis using the method similar to Example 10. Consequently, this was  
15 Mn=8,000 and Mw=16,000. When performing the <sup>1</sup>H-NMR analysis of the PHA obtained using the method similar to Example 10, it was confirmed to be the PHA containing 99% 3-hydroxy-5-(4-vinylphenyl)valeric acid unit and 3-hydroxybutyric acid as the other unit.

20 (Example 23)

200 mL of the M9 medium containing 0.5% (w/v) sodium malate and 0.1% (v/v) n-phenoxy pentane was prepared, placed into a 500 mL volume shaking flask and sterilized by an autoclave.

25 The flask was returned to a room temperature and the *Pseudomonas cichorii* YN2 strain on the agar plate was inoculated, then this was cultured with shaking at

125 strokes/min at 30°C. After 120 hours, the bacteria were recovered by centrifugal separation, washed once with cold methanol and lyophilized.

5 This lyophilized pellet was suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract PHA. After the extract was filtered through a membrane filter with the pore size of 0.45 µm, the filtrate was concentrated using a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the  
10 precipitate was recovered and dried in vacuo to obtain 26 mg of the PHA.

The molecular weight of this PHA was evaluated by gel permeation chromatography (GPC; Tosoh HLC-8220, Column; Tosoh TSK-GEL Super HM-H, Solvent; chloroform,  
15 conversion to polystyrene). Consequently, this was Mn=66,000 and Mw=142,000.

After methanolysis of the PHA obtained was performed according to the conventional method, the analysis by a gas chromatography-mass spectrometer (GC-  
20 MS, Shimadzu QP-5050, EI method) was carried out to identify the methyl-esterified form of the PHA monomer unit. The results are shown in Table 30.

Consequently, as shown in Table 30, the present PHA was identified to be the PHA comprising 3-hydroxy-  
25 5-phenoxyvaleric as a monomer unit.

[Table 30]

Production of PHA Produced in Example 23 and  
Composition of Monomer Unit

Dry cell weight	610 mg/L
Dry polymer weight	130 mg/L
Dry polymer weight/Dry cell weight	21.3%
Composition of monomer unit (peak area ratio)	
3-Hydroxybutyric acid	14.6%
3-Hydroxyvaleric acid	0.1%
3-Hydroxyhexanoic acid	0.2%
3-Hydroxyoctanoic acid	1.1%
3-Hydroxydecanoic acid	0.2%
3-Hydroxydodecanoic acid	1.0%
3-Hydroxydodecenoic acid	1.2%
3-Hydroxy-5-phenoxyvaleric acid	81.6%

(Example 24)

200 mL of the M9 medium containing 0.1% (v/v) n-nonanoic acid and 0.1% (v/v) n-phenoxy pentane was prepared, placed into a 500 mL volume shaking flask and sterilized by an autoclave.

The flask was returned to a room temperature and the *Pseudomonas cichorii* YN2 strain on the agar plate was inoculated, then this was cultured with shaking at 125 strokes/min at 30°C. After 120 hours, the bacteria were recovered by centrifugal separation, washed once with cold methanol and lyophilized.

This lyophilized pellet was suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract

PHA. After the extract was filtered through a membrane filter with the pore size of 0.45  $\mu$ m, the filtrate was concentrated using a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the precipitate was recovered and dried in vacuo to obtain 13 mg of the PHA.

The molecular weight of this PHA was evaluated by gel permeation chromatography (GPC; Tosoh HLC-8220, Column; Tosoh TSK-GEL Super HM-H, Solvent; chloroform, conversion to polystyrene). Consequently, this was  $M_n=51,000$  and  $M_w=130,000$ .

After methanolysis of the PHA obtained was performed according to the conventional method, the analysis by a gas chromatography-mass spectrometer (GC-MS, Shimadzu QP-5050, EI method) was carried out to identify the methyl-esterified form of the PHA monomer unit. The results are shown in Table 31.

Consequently, as shown in Table 31, the present PHA was identified to be the PHA comprising 3-hydroxy-5-phenoxyvaleric acid as a monomer unit.

[Table 31]

Production of PHA Produced in Example 24 and  
Composition of Monomer Unit

Dry cell weight	370 mg/L
Dry polymer weight	65 mg/L
Dry polymer weight/Dry cell weight	17.5%
Composition of monomer unit (peak area ratio)	
3-Hydroxybutyric acid	0.6%
3-Hydroxyvaleric acid	0.0%
3-Hydroxyhexanoic acid	0.2%
3-Hydroxyheptanoic acid	12.4%
3-Hydroxyoctanoic acid	6.1%
3-Hydroxynonanoic acid	59.1%
3-Hydroxydecanoic acid	0.2%
3-Hydroxydodecanoic acid	1.0%
3-Hydroxydodecenoic acid	1.0%
3-Hydroxy-5-phenoxyvaleric acid	19.4%

(Example 25)

200 mL of the M9 medium containing 0.5% (w/v) glucose was prepared, placed into 500 mL volume shaking flask and sterilized by autoclave. The flask was returned to a room temperature and n-amylbenzene sterilized by a filter was added with well stirring so that the concentration is adjusted to 0.1% (v/v), then the *Pseudomonas cichorii* YN2 strain was inoculated and cultured with shaking at 125 stroke/min at 30°C. After 90 hours, the bacteria were recovered by centrifugal separation, washed and lyophilized.

This lyophilized pellet was suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract PHA. After the extract was filtered through a membrane filter with the pore size of 0.45 µm, the filtrate was concentrated using a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the precipitate was recovered and dried in vacuo to obtain 77 mg of the PHA.

The molecular weight of this PHA obtained by performing the GPR analysis using the method similar to Example 16. Consequently, this was  $M_n=51000$ ,  $M_w=102000$ . When performing the  $^1H$ -NMR analysis of the PHA obtained using the method similar to Example 16, it was confirmed to be the PHA containing 71% 3-hydroxy-5-phenylvaleric acid unit and saturated or unsaturated 4 to 12 carbon length 3-hydroxyalkanoic acids as the other unit.

(Example 26)

200 mL of the M9 medium containing 0.5% (w/v) glucose was prepared, placed into 500 mL volume shaking flask and sterilized by autoclave. The flask was returned to a room temperature and n-amylbenzene sterilized by a filter was added with well stirring so that the concentration is adjusted to 0.1% (v/v), then the *Pseudomonas cichorii* YN2 strain was inoculated and cultured with shaking at 125 stroke/min at 30°C. After 90 hours, the bacteria were recovered by centrifugal



separation.

Then, 200 mL of the M9 medium containing 0.5% (w/v) glucose but not containing  $\text{NH}_4\text{Cl}$  as a nitrogen source was prepared, placed into 500 mL volume shaking flask and sterilized by autoclave. The flask was returned to a room temperature and n-amylbenzene sterilized by a filter was added with well stirring so that the concentration is adjusted to 0.1% (v/v), then the recovered bacteria was resuspended in the medium and cultured with shaking at 125 stroke/min at 30°C. After 90 hours, the bacteria were recovered by centrifugal separation, washed once with cold methanol and lyophilized.

This lyophilized pellet was suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract PHA. After the extract was filtered through a membrane filter with the pore size of 0.45  $\mu\text{m}$ , the filtrate was concentrated using a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the precipitate was recovered and dried in vacuo to obtain 92mg of the PHA.

The molecular weight of this PHA obtained by performing the GPR analysis using the method similar to Example 16. Consequently, this was  $M_n=49000$ ,  $M_w=103000$ . When performing the  $^1\text{H-NMR}$  analysis of the PHA obtained using the method similar to Example 16, it was confirmed to be the PHA containing 66%

3-hydroxy-5-phenylvaleric acid unit and saturated or unsaturated 4 to 12 carbon length 3-hydroxyalkanoic acids as the other unit.

(Example 27)

5           200 mL of the M9 medium containing 0.5% (w/v) glucose was prepared, placed into 500 mL volume shaking flask and sterilized by autoclave. The flask was returned to a room temperature and n-amylbenzene sterilized by a filter was added with well stirring so  
10       that the concentration is adjusted to 0.1%(v/v), then the *Pseudomonas cichorii* YN2 strain was inoculated and cultured with shaking at 125 stroke/min at 30°C. After 90 hours, the bacteria were recovered by centrifugal separation.

15           Then, 200 mL of the M9 medium containing 0.5% (w/v) glucose was prepared, placed into 500 mL volume shaking flask and sterilized by autoclave. The flask was returned to a room temperature and n-amylbenzene sterilized by a filter was added with well stirring so  
20       that the concentration is adjusted to 0.1% (v/v), then the recovered bacteria was resuspended in the medium and cultured with shaking at 125 stroke/min at 30°C. After 90 hours, the bacteria were recovered by centrifugal separation, washed once with cold methanol  
25       and lyophilized.

          This lyophilized pellet was suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract

PHA. After the extract was filtered through a membrane filter with the pore size of 0.45  $\mu$ m, the filtrate was concentrated using a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the precipitate was recovered and dried in vacuo to obtain 145mg of the PHA.

The molecular weight of this PHA obtained by performing the GPR analysis using the method similar to Example 16. Consequently, this was  $M_n=48000$ ,  $M_w=96000$ . When performing the  $^1H$ -NMR analysis of the PHA obtained using the method similar to Example 16, it was confirmed to be the PHA containing 72% 3-hydroxy-5-phenylvaleric acid unit and saturated or unsaturated 4 to 12 carbon length 3-hydroxyalkanoic acids as the other unit.

(Example 28)

200 mL of the M9 medium containing 0.5% (w/v) glucose was prepared, placed into 500 mL volume shaking flask and sterilized by autoclave. The flask was returned to a room temperature and n-amylobenzene sterilized by a filter was added with well stirring so that the concentration is adjusted to 0.1%(v/v), then the *Pseudomonas cichorii* YN2 strain was inoculated and cultured with shaking at 125 stroke/min at 30°C. After 90 hours, the bacteria were recovered by centrifugal separation.

Then, 200 mL of the M9 medium but not containing

NH<sub>4</sub>Cl as a nitrogen source was prepared, placed into 500 mL volume shaking flask and sterilized by autoclave. The flask was returned to a room temperature and n-amylbenzene sterilized by a filter was added with well stirring so that the concentration is adjusted to 0.1% (v/v), then the recovered bacteria was resuspended in the medium and cultured with shaking at 125 stroke/min at 30°C. After 90 hours, the bacteria were recovered by centrifugal separation, washed once with cold methanol and lyophilized.

This lyophilized pellet was suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract PHA. After the extract was filtered through a membrane filter with the pore size of 0.45 µm, the filtrate was concentrated using a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the precipitate was recovered and dried vacuo to obtain 64mg of the PHA.

The molecular weight of this PHA obtained by performing the GPR analysis using the method similar to Example 16. Consequently, this was Mn=52000, Mw=99000. When performing the 1H-NMR analysis of the PHA obtained using the method similar to Example 16, it was confirmed to be the PHA containing 73% 3-hydroxy-5-phenylvaleric acid unit and saturated or unsaturated 4 to 12 carbon length 3-hydroxyalkanoic acids as the other unit.

(Example 29)

200 mL of the M9 medium containing 0.5% (w/v) polypeptone was prepared, placed into 500 mL volume shaking flask and sterilized by autoclave. The flask  
5 was returned to a room temperature and n-amylbenzene sterilized by a filter was added with well stirring so that the concentration is adjusted to 0.1%(v/v), then the *Pseudomonas cichorii* YN2 strain was inoculated and cultured with shaking at 125 stroke/min at 30°C. After  
10 48 hours, the bacteria were recovered by centrifugal separation.

Then, 200 mL of the M9 medium containing 0.5% (w/v) glucose but not containing  $\text{NH}_4\text{Cl}$  as a nitrogen source was prepared, placed into 500 mL volume shaking  
15 flask and sterilized by autoclave. The flask was returned to a room temperature and n-amylbenzene sterilized by a filter was added with well stirring so that the concentration is adjusted to 0.1% (v/v), then the recovered bacteria was resuspended in the medium  
20 and cultured with shaking at 125 stroke/min at 30°C. After 90 hours, the bacteria were recovered by centrifugal separation, washed once with cold methanol and lyophilized.

This lyophilized pellet was suspended in 20 mL of  
25 chloroform and stirred at 60°C for 20 hours to extract PHA. After the extract was filtered through a membrane filter with the pore size of 0.45  $\mu\text{m}$ , the filtrate was

concentrated using a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the precipitate was recovered and dried in vacuo to obtain 155mg of the PHA.

5           The molecular weight of this PHA obtained by performing the GPR analysis using the method similar to Example 16. Consequently, this was  $M_n=48000$ ,  $M_w=101000$ . When performing the  $^1H$ -NMR analysis of the PHA obtained using the method similar to Example 16, it  
10       was confirmed to be the PHA containing 78% 3-hydroxy-5-phenylvaleric acid unit and saturated or unsaturated 4 to 12 carbon length 3-hydroxyalkanoic acids as the other unit.

(Example 30)

15           200 mL of the M9 medium containing 0.5% (w/v) polypeptone was prepared, placed into 500 mL volume shaking flask and sterilized by autoclave. The flask was returned to a room temperature and n-amylbenzene sterilized by a filter was added with well stirring so  
20       that the concentration is adjusted to 0.1%(v/v), then the *Pseudomonas cichorii* YN2 strain was inoculated and cultured with shaking at 125 stroke/min at 30°C. After 48 hours, the bacteria were recovered by centrifugal separation.

25           Then, 200 mL of the M9 medium containing 0.5% (w/v) glucose was prepared, placed into 500 mL volume shaking flask and sterilized by autoclave. The flask

was returned to a room temperature and n-amylbenzene  
sterilized by a filter was added with well stirring so  
that the concentration is adjusted to 0.1% (v/v), then  
the recovered bacteria was resuspended in the medium  
5 and cultured with shaking at 125 stroke/min at 30°C.  
After 90 hours, the bacteria were recovered by  
centrifugal separation, washed once with cold methanol  
and lyophilized.

This lyophilized pellet was suspended in 20 mL of  
10 chloroform and stirred at 60°C for 20 hours to extract  
PHA. After the extract was filtered through a membrane  
filter with the pore size of 0.45 µm, the filtrate was  
concentrated using a rotary evaporator, the concentrate  
was reprecipitated in cold methanol, further only the  
15 precipitate was recovered and dried in vacuo to obtain  
110mg of the PHA.

The molecular weight of this PHA obtained by  
performing the GPR analysis using the method similar to  
Example 16. Consequently, this was Mn=46000, Mw=97000.  
20 When performing the 1H-NMR analysis of the PHA obtained  
using the method similar to Example 16, it was  
confirmed to be the PHA containing 91% 3-hydroxy-5-  
phenylvaleric acid unit and saturated or unsaturated 4  
to 12 carbon length 3-hydroxyalkanoic acids as the  
25 other unit.

(Example 31)

200 mL of the M9 medium containing 0.5% (w/v)

polypeptone was prepared, placed into 500 mL volume shaking flask and sterilized by autoclave. The flask was returned to a room temperature and n-amylbenzene sterilized by a filter was added with well stirring so  
5 that the concentration is adjusted to 0.1% (v/v), then the *Pseudomonas cichorii* YN2 strain was inoculated and cultured with shaking at 125 stroke/min at 30°C. After 48 hours, the bacteria were recovered by centrifugal separation.

10 Then, 200 mL of the M9 medium but not containing  $\text{NH}_4\text{Cl}$  as a nitrogen source was prepared, placed into 500 mL volume shaking flask and sterilized by autoclave. The flask was returned to a room temperature and n-amylvenzene sterilized by a filter was added with well  
15 stirring so that the concentration is adjusted to 0.1% (v/v), then the recovered bacteria was resuspended in the medium and cultured with shaking at 125 stroke/min at 30°C. After 90 hours, the bacteria were recovered by centrifugal separation, washed once with cold  
20 methanol and lyophilized.

This lyophilized pellet was suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract PHA. After the extract was filtered through a membrane filter with the pore size of 0.45  $\mu\text{m}$ , the filtrate was  
25 concentrated using a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the precipitate was recovered and dried in vacuo to obtain



41 mg of the PHA.

The molecular weight of this PHA obtained by performing the GPR analysis using the method similar to Example 16. Consequently, this was  $M_n=44000$ ,  $M_w=88000$ .  
5 When performing the  $^1H$ -NMR analysis of the PHA obtained using the method similar to Example 16, it was confirmed to be the PHA containing 95% 3-hydroxy-5-phenylvaleric acid unit and saturated or unsaturated 4 to 12 carbon length 3-hydroxyalkanoic acids as the  
10 other unit.  
(Example 32)

YN2 colonies on M9 medium plate containing 0.1% nonanate were suspended in sterilized physiological saline so that the turbidity at 600nm is adjusted to  
15 0.1. Forty M9 medium plates without carbon source were prepared, the suspension was applied to the plates and cultured at 30°C in nonane atmosphere. After 48 hours, the bacteria were recovered and suspended in 2 mL of physiological saline.

20 Then, 200 mL of the M9 medium containing 0.5 (w/v) glucose but not containing  $NH_4Cl$  as a nitrogen source was prepared, placed into 500 mL volume shaking flask and sterilized by autoclave. The flask was returned to a room temperature and n-amylbenzene sterilized by a  
25 filter was added with well stirring so that the concentration is adjusted to 0.1% (v/v), then the recovered bacteria was resuspended in the medium and

cultured with shaking at 125 stroke/min at 30°C. After 90 hours, the bacteria were recovered by centrifugal separation, washed once with cold methanol and lyophilized.

5           This lyophilized pellet was suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract PHA. After the extract was filtered through a membrane filter with the pore size of 0.45  $\mu$ m, the filtrate was concentrated using a rotary evaporator, the concentrate  
10 was reprecipitated in cold methanol, further only the precipitate was recovered and dried in vacuo to obtain 9 mg of the PHA.

          When performing the <sup>1</sup>H-NMR analysis of the PHA obtained using the method similar to Example 16, it was  
15 confirmed to be the PHA containing 45% 3-hydroxy-5-phenylvaleric acid unit and saturated or unsaturated 4 to 12 carbon length 3-hydroxyalkanoic acids as the other unit.

(Example 33)

20           YN2 colonies on M9 medium plate containing 0.1% nonanate were suspended in sterilized physiological saline so that the turbidity at 600nm is adjusted to 0.1. Forty M9 medium plates without carbon source were prepared, the suspension was applied to the plates and  
25 cultured at 30°C in nonane atmosphere. After 48 hours, the bacteria were recovered and suspended in 2 mL of physiological saline.

Then, 200 mL of the M9 medium containing 0.5% (w/v) glucose was prepared, placed into 500 mL volume shaking flask and sterilized by autoclave. The flask was returned to a room temperature and n-amylobenzene  
5 sterilized by a filter was added with well stirring so that the concentration is adjusted to 0.1% (v/v), then the recovered bacteria was resuspended in the medium and cultured with shaking at 125 stroke/min at 30°C. After 90 hours, the bacteria were recovered by  
10 centrifugal separation, washed once with cold methanol and lyophilized.

This lyophilized pellet was suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract PHA. After the extract was filtered through a membrane  
15 filter with the pore size of 0.45 µm, the filtrate was concentrated using a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the precipitate was recovered and dried in vacuo to obtain 83 mg of the PHA.

20 When performing the <sup>1</sup>H-NMR analysis of the PHA obtained using the method similar to Example 16, it was confirmed to be the PHA containing 13% 3-hydroxy-5-phenylvaleric acid unit and saturated or unsaturated 4 to 12 carbon length 3-hydroxyalkanoic acids as the  
25 other unit.  
(Example 34)

200 mL of the M9 medium containing 0.5% (w/v)

glucose was prepared, placed into 500 mL volume shaking flask and sterilized by autoclave. The flask was returned to a room temperature and n-hexanophenon sterilized by a filter was added with well stirring so  
5 that the concentration is adjusted to 0.1% (v/v), then the *Pseudomonas cichorii* YN2 strain was inoculated and cultured with shaking at 125 stroke/min at 30°C. After 90 hours, the bacteria were recovered by centrifugal separation.

10 Then, 200 mL of the M9 medium containing 0.5% (w/v) glucose but not containing  $\text{NH}_4\text{Cl}$  as a nitrogen source was prepared, placed into 500 mL volume shaking flask and sterilized by autoclave. The flask was returned to a room temperature and n-hexanophenon  
15 sterilized by a filter was added with well stirring so that the concentration is adjusted to 0.1% (v/v), then the recovered bacteria was resuspended in the medium and cultured with shaking at 125 stroke/min at 30°C. After 90 hours, the bacteria were recovered by  
20 centrifugal separation, washed once with cold methanol and lyophilized.

This lyophilized pellet was suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract PHA. After the extract was filtered through a membrane  
25 filter with the pore size of 0.45  $\mu\text{m}$ , the filtrate was concentrated using a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the

precipitate was recovered and dried in vacuo to obtain 51 mg of the PHA.

The molecular weight of this PHA obtained by performing the GPR analysis using the method similar to Example 16. Consequently, this was  $M_n=88000$ ,  $M_w=238000$ . When performing the  $^1H$ -NMR analysis of the PHA obtained using the method similar to Example 16, it was confirmed to be the PHA containing 38% 3-hydroxy-5-benzoylvaleric acid unit and saturated or unsaturated 4 to 12 carbon length 3-hydroxyalkanoic acids as the other unit.

(Example 35)

200 mL of the M9 medium containing 0.5% (w/v) glucose was prepared, placed into 500 mL volume shaking flask and sterilized by autoclave. The flask was returned to a room temperature and n-hexanophenon sterilized by a filter was added with well stirring so that the concentration is adjusted to 0.1% (v/v), then the *Pseudomonas cichorii* YN2 strain was inoculated and cultured with shaking at 125 stroke/min at 30°C. After 90 hours, the bacteria were recovered by centrifugal separation.

Then, 200 mL of the M9 medium containing 0.5% (w/v) glucose was prepared, placed into 500 mL volume shaking flask and sterilized by autoclave. The flask was returned to a room temperature and n-hexanophenon sterilized by a filter was added with well stirring so

that the concentration is adjusted to 0.1% (v/v), then the recovered bacteria was resuspended in the medium and cultured with shaking at 125 stroke/min at 30°C. After 90 hours, the bacteria were recovered by  
5 centrifugal separation, washed once with cold methanol and lyophilized.

This lyophilized pellet was suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract PHA. After the extract was filtered through a membrane  
10 filter with the pore size of 0.45 µm, the filtrate was concentrated using a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the precipitate was recovered and dried in vacuo to obtain 44 mg of the PHA.

15 The molecular weight of this PHA obtained by performing the GPR analysis using the method similar to Example 16. Consequently, this was  $M_n=107000$ ,  $M_w=203000$ . When performing the <sup>1</sup>H-NMR analysis of the PHA obtained using the method similar to Example 16, it  
20 was confirmed to be the PHA containing 32% 3-hydroxy-5-benzoylvaleric acid unit and saturated or unsaturated 4 to 12 carbon length 3-hydroxyalkanoic acids as the other unit.

(Example 36)

25 200 mL of the M9 medium containing 0.5% (w/v) glucose was prepared, placed into 500 mL volume shaking flask and sterilized by autoclave. The flask was

returned to a room temperature and n-phenoxy-pentane  
sterilized by a filter was added with well stirring so  
that the concentration is adjusted to 0.1% (v/v), then  
the *Pseudomonas cichorii* YN2 strain was inoculated and  
5 cultured with shaking at 125 stroke/min at 30°C. After  
90 hours, the bacteria were recovered by centrifugal  
separation.

Then, 200 mL of the M9 medium containing 0.5%  
(w/v) glucose but not containing  $\text{NH}_4\text{Cl}$  as a nitrogen  
10 source was prepared, placed into 500 mL volume shaking  
flask and sterilized by autoclave. The flask was  
returned to a room temperature and n-phenoxy-pentane  
sterilized by a filter was added with well stirring so  
that the concentration is adjusted to 0.1% (v/v), then  
15 the recovered bacteria was resuspended in the medium  
and cultured with shaking at 125 stroke/min at 30°C.  
After 90 hours, the bacteria were recovered by  
centrifugal separation, washed once with cold methanol  
and lyophilized.

20 This lyophilized pellet was suspended in 20 mL of  
chloroform and stirred at 60°C for 20 hours to extract  
PHA. After the extract was filtered through a membrane  
filter with the pore size of 0.45  $\mu\text{m}$ , the filtrate was  
concentrated using a rotary evaporator, the concentrate  
25 was reprecipitated in cold methanol, further only the  
precipitate was recovered and dried in vacuo to obtain  
54 mg of the PHA.

The molecular weight of this PHA obtained by performing the GPR analysis using the method similar to Example 16. Consequently, this was  $M_n=72000$ ,  $M_w=158000$ . When performing the  $^1H$ -NMR analysis of the PHA obtained using the method similar to Example 16, it was confirmed to be the PHA containing 60% 3-hydroxy-5-phenoxyvaleric acid unit and saturated or unsaturated 4 to 12 carbon length 3-hydroxyalkanoic acids as the other unit.

10 (Example 37)

200 mL of the M9 medium containing 0.5% (w/v) glucose was prepared, placed into 500 mL volume shaking flask and sterilized by autoclave. The flask was returned to a room temperature and n-phenoxy-pentane sterilized by a filter was added with well stirring so that the concentration is adjusted to 0.1% (v/v), then the *Pseudomonas cichorii* YN2 strain was inoculated and cultured with shaking at 125 stroke/min at 30°C. After 90 hours, the bacteria were recovered by centrifugal separation.

25 Then, 200 mL of the M9 medium containing 0.5% (w/v) glucose was prepared, placed into 500 mL volume shaking flask and sterilized by autoclave. The flask was returned to a room temperature and n-phenoxy-pentane sterilized by a filter was added with well stirring so that the concentration is adjusted to 0.1% (v/v), then the recovered bacteria was resuspended in the medium



and cultured with shaking at 125 stroke/min at 30°C. After 90 hours, the bacteria were recovered by centrifugal separation, washed once with cold methanol and lyophilized.

5        This lyophilized pellet was suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract PHA. After the extract was filtered through a membrane filter with the pore size of 0.45 µm, the filtrate was concentrated using a rotary evaporator, the concentrate  
10       was reprecipitated in cold methanol, further only the precipitate was recovered and dried in vacuo to obtain 42 mg of the PHA.

      The molecular weight of this PHA obtained by performing the GPR analysis using the method similar to  
15       Example 16. Consequently, this was  $M_n=78000$ ,  $M_w=156000$ . When performing the  $^1H$ -NMR analysis of the PHA obtained using the method similar to Example 16, it was confirmed to be the PHA containing 60 % 3-hydroxy-5-phenoxyvaleric acid unit and saturated or unsaturated  
20       4 to 12 carbon length 3-hydroxyalkanoic acids as the other unit.

(Example 38)

      200 mL of the M9 medium containing 0.5 % (w/v) glucose was prepared, placed into 500 mL volume shaking  
25       flask and sterilized by autoclave. The flask was returned to a room temperature and n-amylobenzene sterilized by a filter was added with well stirring so

that the concentration is adjusted to 0.1% (v/v), then the *Pseudomonas cichorii* YN2 strain was inoculated and cultured with shaking at 125 stroke/min at 30°C. When turbidity at 600 nm became 0.1, dicyclopropylketone was added with well stirring so that the concentration is adjusted to 0.05 % (v/v) and continued shake culturing. After 90 hours, the bacteria were recovered by centrifugal separation, washed and lyophilized.

This lyophilized pellet was suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract PHA. After the extract was filtered through a membrane filter with the pore size of 0.45  $\mu$ m, the filtrate was concentrated using a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the precipitate was recovered and dried in vacuo to obtain 54 mg of the PHA.

The molecular weight of this PHA obtained by performing the GPR analysis using the method similar to Example 16. Consequently, this was  $M_n=30000$ ,  $M_w=63000$ . When performing the  $^1H$ -NMR analysis of the PHA obtained using the method similar to Example 16, it was confirmed to be the PHA containing 37% 3-hydroxy-5-phenylvaleric acid unit and saturated or unsaturated 4 to 12 carbon length 3-hydroxyalkanoic acids as the other unit.

(Example 39)

200 mL of the M9 medium containing 0.5 % (w/v)

polypeptone was prepared, place into 500 mL volume shaking flask and sterilized by an autoclave. The flask was returned to a room temperature and n-amylbenzene sterilized by a filter was added with well stirring so that the concentration is adjusted to 0.1 % (v/v), then the *Pseudomonas cichorii* YN2 strain was inoculated and cultured with shaking at 125 stroke/min at 30°C. When turbidity at 600 nm became 0.1, dicyclopropylketone was added with well stirring so that the concentration is adjusted to 0.05 % (v/v) and continued shake culturing. After 48 hours, the bacteria were recovered by centrifugal separation, washed and lyophilized.

This lyophilized pellet was suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract PHA. After the extract was filtered through a membrane filter with the pore size of 0.45  $\mu\text{m}$ , the filtrate was concentrated using a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the precipitate was recovered and dried in vacuo to obtain 67 mg of the PHA.

The molecular weight of this PHA obtained by performing the GPR analysis using the method similar to Example 16. Consequently, this was  $M_n=30000$ ,  $M_w=66000$ . When performing the  $^1\text{H-NMR}$  analysis of the PHA obtained using the method similar to Example 16, it was confirmed to be the PHA containing 79 % 3-hydroxy-5-phenylvaleric acid unit and 3-hydroxybutyric acid as the other unit.

(Example 40)

200 mL of the M9 medium containing 0.5 % (w/v) glucose was prepared, placed into 500 mL volume shaking flask and sterilized by an autoclave. The flask was returned to a room temperature and n-amylbenzene sterilized by a filter was added with well stirring so that the concentration is adjusted to 0.1 % (v/v), then the *Pseudomonas cichorii* YN2 strain was inoculated and cultured with shaking at 125 stroke/min at 30°C. When turbidity at 600 nm became 0.1, dicyclopropylketone was added with well stirring so that the concentration is adjusted to 0.05 % (v/v), then the shake culturing was continued. After 14 hours, the bacteria were recovered by centrifugal separation.

Then, 200 mL of the M9 medium containing 0.5 % (w/v) glucose but not containing  $\text{NH}_4\text{Cl}$  as a nitrogen source was prepared, placed into 500 mL volume shaking flask and sterilized by an autoclave. The flask was returned to a room temperature and n-amylbenzene sterilized by a filter was added with well stirring so that the concentration is adjusted to 0.1 % (v/v), then the recovered bacteria was resuspended in the medium and cultured with shaking at 125 stroke/min at 30°C. After 90 hours, the bacteria were recovered by centrifugal separation, washed once with cold methanol and lyophilized.

This lyophilized pellet was suspended in 20 mL of

chloroform and stirred at 60°C for 20 hours to extract PHA. After the extract was filtered through a membrane filter with the pore size of 0.45  $\mu$ m, the filtrate was concentrated using a rotary evaporator, the concentrate was reprecipitated in  
5 cold methanol, further only the precipitate was recovered and dried in vacuo to obtain 12 mg of the PHA.

The molecular weight of this PHA obtained by performing the GPR analysis using the method similar to Example 16. Consequently, this was  $M_n=50000$ ,  $M_w=110000$ . When performing  
10 the  $^1H$ -NMR analysis of the PHA obtained using the method similar to Example 16, it was confirmed to be the PHA containing 86 % 3-hydroxy-5-phenylvaleric acid unit and saturated or unsaturated 4 to 12 length 3-hydroxyalkanoic acids as the other unit.

15 (Example 41)

200 mL of the M9 medium containing 0.5 % (w/v) glucose was prepared, placed into 500 mL volume shaking flask and sterilized by an autoclave. The flask was returned to a room temperature and n-amylbenzene sterilized by a filter was  
20 added with well stirring so that the concentration is adjusted 0.1 % (v/v), then the *Pseudomonas cichorii* YN2 strain was inoculated and cultured with shaking at 125 stroke/min at 30°C. When turbidity at 600 nm became 0.1, dicyclopropylketone was added with well stirring so that the  
25 concentration is adjusted to 0.05 % (v/v), then the shake

culturing was continued. After 14 hours, the bacteria were recovered by centrifugal separation.

Then, 200 mL of the M9 medium containing 0.5 % (w/v) glucose was prepared, placed into 500 mL volume shaking flask and sterilized by an autoclave. The flask was returned to a room temperature and n-amylbenzene sterilized by a filter was added with well stirring so that the concentration is adjusted to 0.1 % (v/v), then the recovered bacteria was resuspended in the medium and cultured with shaking at 125 stroke/min at 30°C. After 90 hours, the bacteria were recovered by centrifugal separation, washed once with cold methanol and lyophilized.

This lyophilized pellet was suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract PHA. After the extract was filtered through a membrane filter with the pore size of 0.45  $\mu$ m, the filtrate was concentrated using a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the precipitate was recovered and dried in vacuo to obtain 87 mg of the PHA.

The molecular weight of this PHA obtained by performing the GPR analysis using the method similar to Example 16. Consequently, this was  $M_n=53000$ ,  $M_w=106000$ . When performing the  $^1H$ -NMR analysis of the PHA obtained using the method similar to Example 16, it was confirmed to be the PHA containing 86% 3-hydroxy-5-phenylvaleric acid unit and

saturated or unsaturated 4 to 12 carbon length 3-hydroxyalkanoic acids as the other unit.

(Example 42)

200 mL of the M9 medium containing 0.5 % (w/v) polypeptone was prepared, placed into 500 mL volume shaking flask and sterilized by an autoclave. The flask was returned to a room temperature and n-amylbenzene sterilized by a filter was added with well stirring so that the concentration is adjusted to 0.1% (v/v), then the *Pseudomonas cichorii* YN2 strain was inoculated and cultured with shaking at 125 stroke/min at 30°C. When turbidity at 600 nm became 0.1, dicyclopropylketone was added with well stirring so that the concentration is adjusted to 0.05% (v/v), then the shake culturing was continued. After 14 hours, the bacteria were recovered by centrifugal separation.

Then, 200 mL of the M9 medium containing 0.5% (w/v) glucose but not containing  $\text{NH}_4\text{Cl}$  as a nitrogen source was prepared, placed into 500 mL volume shaking flask and sterilized by an autoclave. Then flask was returned to a room temperature and n-amylbenzene sterilized by a filter was added with well stirring so that the concentration is adjusted to 0.1% (v/v), then the recovered bacteria was resuspended in the medium

and cultured with shaking at 125 stroke/min at 30°C. After 90 hours, the bacteria were recovered by centrifugal separation, washed once with cold methanol and lyophilized.

5           This lyophilized pellet was suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract PHA. After the extract was filtered through a membrane filter with the pore size of 0.45 µm, the filtrate was concentrated using a rotary evaporator, the concentrate  
10           was reprecipitated in cold methanol, further only the precipitate was recovered and dried in vacuo to obtain 150mg of the PHA.

          The molecular weight of this PHA obtained by performing the GPR analysis using the method similar to  
15           Example 16. Consequently, this was Mn=66000, Mw=145000. When performing the 1H-NMR analysis of the PHA obtained using the method similar to Example 16, it was confirmed to be the PHA containing 83% 3-hydroxy-5-phenylvaleric acid unit and saturated or unsaturated 4  
20           to 12 carbon length 3-hydroxyalkanoic acids as the other unit.

(Example 43)

          200 mL of the M9 medium containing 0.5% (w/v) polypeptone was prepared, placed into 500 mL volume  
25           shaking flask and sterilized by autoclave. The flask was returned to a room temperature and n-amylbenzene sterilized by a filter was added with well stirring so



that the concentration is adjusted to 0.1% (v/v), then the *Pseudomonas cichorii* YN2 strain was inoculated and cultured with shaking at 125 stroke/min at 30°C. When turbidity at 600 nm became 0.1, dicyclopropylketone was added with well stirring so that the concentration is adjusted to 0.05% (v/v), then the shake culturing was continued. After 14 hours, the bacteria were recovered by centrifugal separation.

Then 200 mL of the M9 medium containing 0.5% (w/v) glucose was prepared, placed into 500 mL volume shaking flask and sterilized by autoclave. The flask was returned to a room temperature and n-amylvenzene sterilized by a filter was added with well stirring so that the concentration is adjusted to 0.1% (v/v), then the recovered bacteria was resuspended in the medium and cultured with shaking at 125 stroke/min at 30°C. After 90 hours, the bacteria were recovered by centrifugal separation, washed once with cold methanol and lyophilized.

This lyophilized pellet was suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract PHA. After the extract was filtered through a membrane filter with the pore size of 0.45 µm, the filtrate was concentrated using a rotary evaporator; the concentrate was reprecipitated in cold methanol, further only the precipitate was recovered and dried in vacuo to obtain 120mg of the PHA.

The molecular weight of this PHA obtained by performing the GPR analysis using the method similar to Example 16. Consequently, this was  $M_n=56000$ ,  $M_w=112000$ . When performing the  $^1H$ -NMR analysis of the PHA obtained using the method  
5 similar to Example 16, it was confirmed to be the PHA containing 91% 3-hydroxy-5-phenylvaleric acid unit and saturated or unsaturated 4 to 12 carbon length 3-hydroxyalkanoic acids as the other unit.

(Example 44)

10 200 mL of the M9 medium containing 0.5% (w/v) glucose was prepared, placed into 500 mL volume shaking flask and sterilized by autoclave. The flask was returned to a room temperature and the *Pseudomonas cichorii* YN2 strain was inoculated and cultured with shaking at 125 stroke/min at  
15 30°C. When turbidity at 600 nm became 0.1, dicyclopropylketone was added with well stirring so that the concentration is adjusted to 0.05% (v/v), then the shake culturing was continued. After 14 hours, the bacteria were recovered by centrifugal separation.

20 Then, 200 mL of the M9 medium containing 0.5% (w/v) glucose but not containing  $HN_4Cl$  as a nitrogen source was prepared, placed into 500 mL volume shaking flask and sterilized by autoclave. The flask was returned to a room temperature and n-amybenzene  
25 sterilized by a filter was added with well stirring so

that the concentration is adjusted to 0.1% (v/v), then the recovered bacteria was resuspended in the medium and cultured with shaking at 125 stroke/min at 30°C. After 90 hours, the bacteria were recovered by  
5 centrifugal separation, washed once with cold methanol and lyophilized.

This lyophilized pellet was suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract PHA. After the extract was filtered through a membrane  
10 filter with the pore size of 0.45  $\mu$ m, the filtrate was concentrated using a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the precipitate was recovered and dried in vacuo to obtain 12mg of the PHA.

15 The molecular weight of this PHA obtained by performing the GPR analysis using the method similar to Example 16. Consequently, this was  $M_n=44000$ ,  $M_w=119000$ . When performing the  $^1H$ -NMR analysis of the PHA obtained using the method similar to Example 16, it  
20 was confirmed to be the PHA containing 87% 3-hydroxy-5-phenylvaleric acid unit and saturated or unsaturated 4 to 12 carbon length 3-hydroxyalkanoic acids as the other unit.

(Example 45)

25 200 mL of the M9 medium containing 0.5% (w/v) glucose was prepared, placed into 500 mL volume shaking flask and sterilized by autoclave. The flask was

returned to a room temperature and the *Pseudomonas*  
cichorii YN2 strain was inoculated and cultured with  
shaking at 125 stroke/min at 30°C. When turbidity at  
600 nm became 0.1, dicyclopropylketone was added with  
5 well stirring so that the concentration is adjusted to  
0.05% (v/v), then the shake culturing was continued.  
After 14 hours, the bacteria were recovered by  
centrifugal separation.

Then, 200 mL of the M9 medium containing 0.5%  
10 (w/v) glucose was prepared, placed into 500 mL volume  
shaking flask and sterilized by autoclave. The flask  
was returned to a room temperature and n-amylbenzene  
sterilized by a filter was added with well stirring so  
that the concentration is adjusted to 0.1% (v/v), then  
15 the recovered bacteria was resuspended in the medium  
and cultured with shaking at 125 stroke/min at 30°C.  
After 90 hours, the bacteria were recovered by  
centrifugal separation, washed once with cold methanol  
and lyophilized.

20 This lyophilized pellet was suspended in 20 mL of  
chloroform and stirred at 60°C for 20 hours to extract  
PHA. After the extract was filtered through a membrane  
filter with the pore size of 0.45 µm, the filtrate was  
concentrated using a rotary evaporator, the concentrate  
25 was reprecipitated in cold methanol, further only the  
precipitate was recovered and dried in vacuo to obtain  
47mg of the PHA.

The molecular weight of this PHA obtained by performing the GPR analysis using the method similar to Example 16. Consequently, this was  $M_n=56000$ ,  $M_w=118000$ . When performing the  $^1H$ -NMR analysis of the PHA obtained using the method similar to Example 16, it was confirmed to be the PHA containing 33% 3-hydroxy-5-phenylvaleric acid unit and saturated or unsaturated 4 to 12 carbon length 3-hydroxyalkanoic acids as the other unit.

10 (Example 46)

200 mL of the M9 medium containing 0.5% (w/v) polypeptone was prepared, placed into 500 mL volume shaking flask and sterilized by autoclave. The flask was returned to a room temperature and the *Pseudomonas cichorii* YN2 strain was inoculated and cultured with shaking 125 stroke/min at 30°C. When turbidity at 600 nm became 0.1, dicyclopropylketone was added with well stirring so that the concentration is adjusted to 0.05% (v/v), then the shake culturing was continued. After 20 14 hours, the bacteria were recovered by centrifugal separation.

Then, 200 mL of the M9 medium containing 0.5% (w/v) glucose but not containing  $NH_4Cl$  as a nitrogen source was prepared, placed into 500 mL volume shaking flask and sterilized by autoclave. The flask was returned to a room temperature and n-amylbenzene sterilized by a filter was added with well stirring so

that the concentration is adjusted to 0.1% (v/v), then the recovered bacteria was resuspended in the medium and cultured with shaking at 125 stroke/min at 30°C. After 90 hours, the bacteria were recovered by  
5 centrifugal separation, washed once with cold methanol and lyophilized.

This lyophilized pellet was suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract PHA. After the extract was filtered through a membrane  
10 filter with the pore size of 0.45 µm, the filtrate was concentrated using a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the precipitate was recovered and dried in vacuo to obtain 150mg of the PHA.

15 The molecular weight of the PHA obtained by performing the GPR analysis using the method similar to Example 16. Consequently, this was  $M_n=64000$ ,  $M_w=134000$ . When performing the  $^1H$ -NMR analysis of the PHA obtained using the method similar to Example 16, it  
20 was confirmed to be the PHA containing 77% 3-hydroxy-5-phenylvaleric acid unit and saturated or unsaturated 4 to 12 carbon length 3-hydroxyalkanoic acids as the other unit.

(Example 47)

25 200 mL of the M9 medium containing 0.5% (w/v) polypeptone was prepared, placed into 500 mL volume shaking flask and sterilized by autoclave. The flask

was returned to a room temperature and the *Pseudomonas cichorii* YN2 strain was inoculated and cultured with shaking at 125 stroke/min at 30°C. When turbidity at 600 nm became 0.1, dicyclopropylketone was added with well stirring so that the concentration is adjusted to 0.05% (v/v), then the shake culturing was continued. After 14 hours, the bacteria were recovered by centrifugal separation.

Then, 200 mL of the M9 medium containing 0.5% (w/v) glucose was prepared, placed into 500 mL volume shaking flask and sterilized by autoclave. The flask was returned to a room temperature and n-amybenzene sterilized by a filter was added with well stirring so that the concentration is adjusted to 0.1% (v/v), then the recovered bacteria was resuspended in the medium and cultured with shaking at 125 stroke/min at 30°C. After 90 hours, the bacteria were recovered by centrifugal separation, washed once with cold methanol and lyophilized.

This lyophilized pellet was suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract PHA. After the extract was filtered through a membrane filter with the pore size of 0.45 µm, the filtrate was concentrated using a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the precipitate was recovered and dried in vacuo to obtain 117mg of the PHA.

The molecular weight of this PHA obtained by performing the GPR analysis using the method similar to Example 16. Consequently, this was  $M_n=63000$ ,  $M_w=126000$ . When performing the  $^1H$ -NMR analysis of the PHA obtained using the method similar to Example 16, it was confirmed to be the PHA containing 83% 3-hydroxy-5-phenylvaleric acid unit and saturated or unsaturated 4 to 12 carbon length 3-hydroxyalkanoic acids as the other unit.

(Example 48)

200 mL of the M9 medium containing 0.5% (w/v) glucose was prepared, placed into 500 mL volume shaking flask and sterilized by autoclave. The flask was returned to a room temperature and n-amylbenzene sterilized by a filter was added with well stirring so that the concentration is adjusted to 0.1% (v/v), then the *Pseudomonas cichorii* YN2 strain was inoculated and cultured with shaking at 125 stroke/min at 30°C. When turbidity at 600nm became 0.1, dicyclopropylketone was added with well stirring so that the concentration is adjusted to 0.05% (v/v), then the shake culturing was continued. After 14 hours, the bacteria were recovered by centrifugal separation.

Then, 200 mL of the M9 medium containing 0.5% (w/v) glucose but not containing  $NH_4Cl$  as a nitrogen source was prepared, placed into 500 mL volume shaking flask and sterilized by autoclave. The flask was



returned to a room temperature and n-amylbenzene  
sterilized by a filter was added with well stirring so  
that the concentration is adjusted to 0.1% (v/v),  
dicyclopropylketone was added with well stirring so  
5 that the concentration is adjusted to 0.05% (v/v), then  
the recovered bacteria was resuspended in the medium  
and cultured with shaking at 125 stroke/min at 30°C.  
After 90 hours, the bacteria were recovered by  
centrifugal separation, washed once with cold methanol  
10 and lyophilized.

This lyophilized pellet was suspended in 20 mL of  
chloroform and stirred at 60°C for 20 hours to extract  
PHA. After the extract was filtered through a membrane  
filter with the pore size of 0.45  $\mu$ m, the filtrate was  
15 concentrated using a rotary evaporate, the concentrate  
was reprecipitated in cold methanol, further only the  
precipitate was recovered and dried in vacuo to obtain  
3mg of the PHA.

The molecular weight of this PHA obtained by  
20 performing the GPR analysis using the method similar to  
Example 16. Consequently, this was  $M_n=43000$ ,  $M_w=90000$ .  
When performing the  $^1H$ -NMR analysis of the PHA obtained  
using the method similar to Example 16, it was  
confirmed to be the PHA containing 88% 3-hydroxy-5-  
25 phenylvaleric acid unit and saturated or unsaturated 4  
to 12 carbon length 3-hydroxyalkanoic acids as the  
other unit.

(Example 49)

200 mL of the M9 medium containing 0.5% (w/v) glucose was prepared, placed into 500 mL volume shaking flask and sterilized by an autoclave. The flask was returned to a room temperature and n-amylbenzene sterilized by a filter was added with well stirring so that the concentration is adjusted to 0.1%(v/v), then the *Pseudomonas cichorii* YN2 strain was inoculated and cultured with shaking at 125 stroke/min at 30°C. When turbidity at 600 nm became 0.1, dicyclopropylketone was added with well stirring so that the concentration is adjusted to 0.05% (v/v), then the shake culturing was continued. After 14 hours, the bacteria were recovered by centrifugal separation.

Then, 200 mL of the M9 medium containing 0.5% (w/v) glucose was prepared, placed into 500 mL volume shaking flask and sterilized by an autoclave. The flask was returned to a room temperature and n-amylbenzene sterilized by a filter was added with well stirring so that the concentration is adjusted to 0.1% (v/v), dicyclopropylketone was added with well stirring so that the concentration is adjusted to 0.05% (v/v), then the recovered bacteria was resuspended in the medium and cultured with shaking at 125 stroke/min at 30°C. After 90 hours, the bacteria were recovered by centrifugal separation, washed once with cold methanol and lyophilized.

This lyophilized pellet was suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract PHA. After the extract was filtered through a membrane filter with the pore size of 0.45  $\mu$ m, the filtrate was concentrated using a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the precipitate was recovered and dried in vacuo to obtain 54mg of the PHA.

The molecular weight of this PHA obtained by performing the GPR analysis using the method similar to Example 16.

Consequently, this was Mn=30000, Mw=66000. When performing the 1H-NMR analysis of the PHA obtained using the method similar to Example 16, it was confirmed to be the PHA containing 76% 3-hydroxy-5-phenylvaleric acid unit and saturated or unsaturated 4 to 12 carbon length 3-hydroxyalkanoic acids as the other unit.

(Example 50)

200 mL of the M9 medium containing 0.5% (w/v) glucose was prepared, placed into 500 mL volume shaking flask and sterilized by an autoclave. The flask was returned to a room temperature and the *Pseudomonas cichorii* YN2 strain was inoculated and cultured with shaking at 125 stroke/min at 30°C. When turbidity at 600nm became 0.1, dicyclopropylketone was added with well stirring so that the concentration is adjusted to 0.05% (v/v), then the shake culturing was continued.

After 14 hours, the bacteria were recovered by centrifugal separation.

Then, 200mL of the M9 medium containing 0.5% (w/v) glucose but not containing  $\text{NH}_4\text{Cl}$  as a nitrogen source  
5 was prepared, placed into 500mL volume shaking flask and sterilized by autoclave. The flask was returned to a room temperature and n-amylbenzene sterilized by a filter was added with well stirring so that the concentration is adjusted to 0.1% (v/v),  
10 dicyclopropylketone was added with well stirring so that the concentration is adjusted to 0.05% (v/v), then the recovered bacteria was resuspended in the medium and cultured with shaking at 125 stroke/min at 30°C. After 90 hours, the bacteria were recovered by  
15 centrifugal separation, washed once with cold methanol and lyophilized.

This lyophilized pellet was suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract PHA. After the extract was filtered through a membrane  
20 filter with the pore size of 0.45  $\mu\text{m}$ , the filtrate was concentrated using a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the precipitate was recovered and dried in vacuo to obtain 5mg of the PHA.

25 The molecular weight of this PHA obtained by performing the GPR analysis using the method similar to Example 16. Consequently, this was  $\text{Mn}=40000$ ,  $\text{Mw}=84000$ .

When performing the <sup>1</sup>H-NMR analysis of the PHA obtained using the method similar to Example 16, it was confirmed to be the PHA containing 87% 3-hydroxy-5-phenylvaleric acid unit and saturated or unsaturated 4 to 12 carbon length 3-

5 hydroxyalkanoic acids as the other unit.

(Example 51)

200 mL of the M9 medium containing 0.5% (w/v) glucose was prepared, placed into 500 ml volume shaking flask and sterilized by an autoclave. The flask was returned to a room  
10 temperature and the *Pseudomonas cichorii* YN2 strain was inoculated and cultured with shaking at 125 stroke/min at 30°C. When turbidity at 600nm became 0.1, dicyclopropylketone was added with well stirring so that the concentration is adjusted to 0.05% (v/v), then the shake  
15 culturing was continued. After 14 hours, the bacteria were recovered by centrifugal separation.

Then, 200 mL of the M9 medium containing 0.5% (w/v) glucose was prepared, placed into 500 mL volume shaking flask and sterilized by an autoclave. The flask was returned to a  
20 room temperature and n-amylbenzene sterilized by a filter was added with well stirring so that the concentration is adjusted to 0.1% (v/v), dicyclopropylketone was added with well stirring so that the concentration is adjusted to 0.05% (v/v), then the recovered bacteria was resuspended in the medium and  
25 cultured with shaking at 125 stroke/min at 30°C. After 90 hours, the bacteria were recovered by centrifugal separation,

washed once with cold methanol and lyophilized.

This lyophilized pellet was suspended in 20 mL of chloroform and stirred at 60°C for 20 hours to extract PHA. After the extract was filtered through a membrane filter with the pore size of 0.45  $\mu$ m, the filtrate was concentrated using a rotary evaporator, the concentrate was reprecipitated in cold methanol, further only the precipitate was recovered and dried in vacuo to obtain 26mg of the PHA.

The molecular weight of this PHA obtained by performing the GPR analysis using the method similar to Example 16. Consequently, this was  $M_n=43000$ ,  $M_w=77000$ . When performing the  $^1H$ -NMR analysis of the PHA obtained using the method similar to Example 16, it was confirmed to be the PHA containing 30% 3-hydroxy-5-phenylvaleric acid unit and saturated or unsaturated 4 to 12 carbon length 3-hydroxyalkanoic acids as the other unit.